

Supplementary Information

The role of solid solutions in iron phosphate-based electrodes for selective electrochemical lithium extraction

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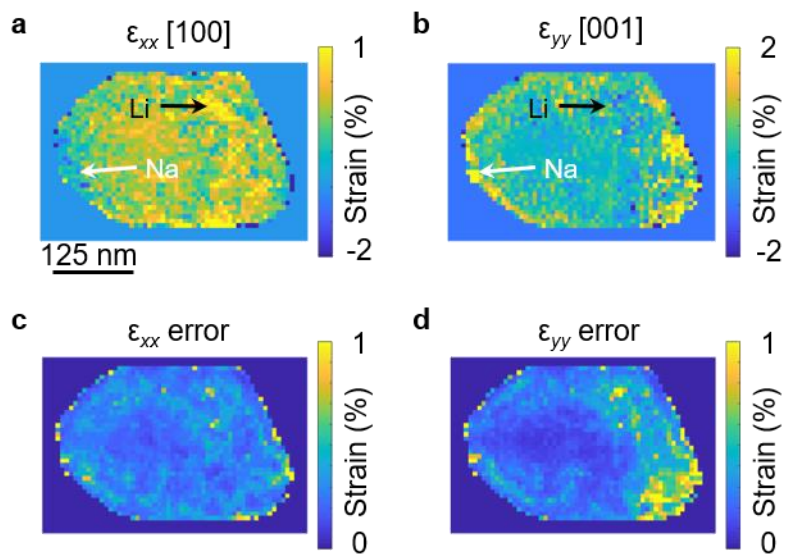
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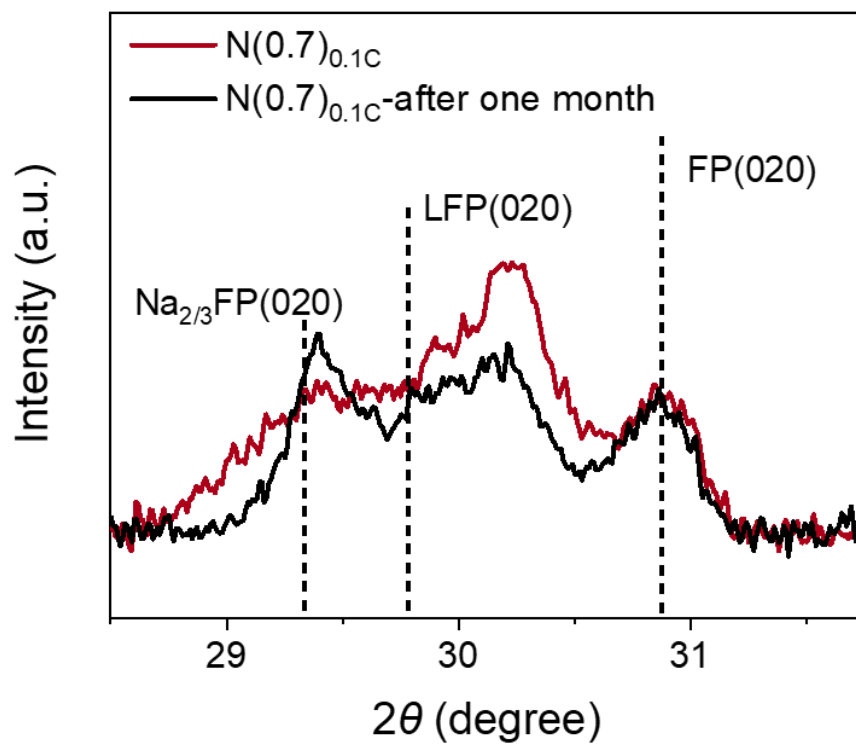
³Department of Materials Science and Engineering, University of Illinois at Urbana-Champaign, Urbana, IL 61801, USA

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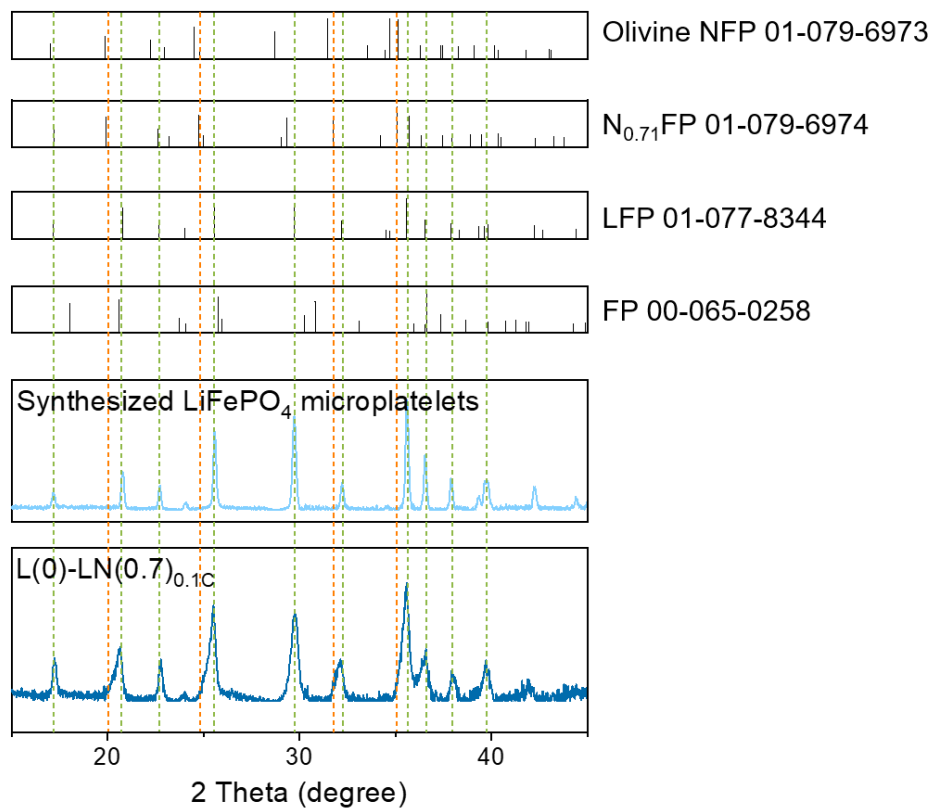
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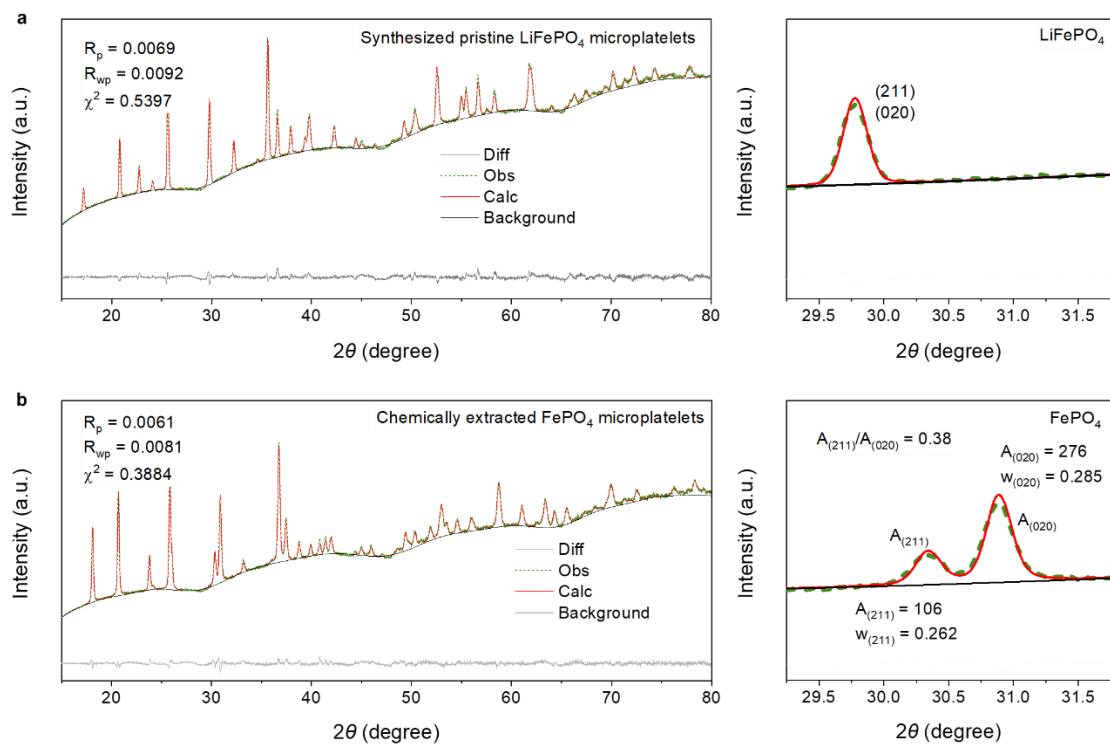
Supplementary Figure 1 Strain maps of the LN(0.7)_{0.1}C particle along ϵ_{xx} [100] and ϵ_{yy} [001] directions converted from the lattice spacing maps with corresponding strain error. The measurement error is converted from uncertainty of diffraction peak detection. (Arrows are a guide-to-the-eye for the phase identification.)



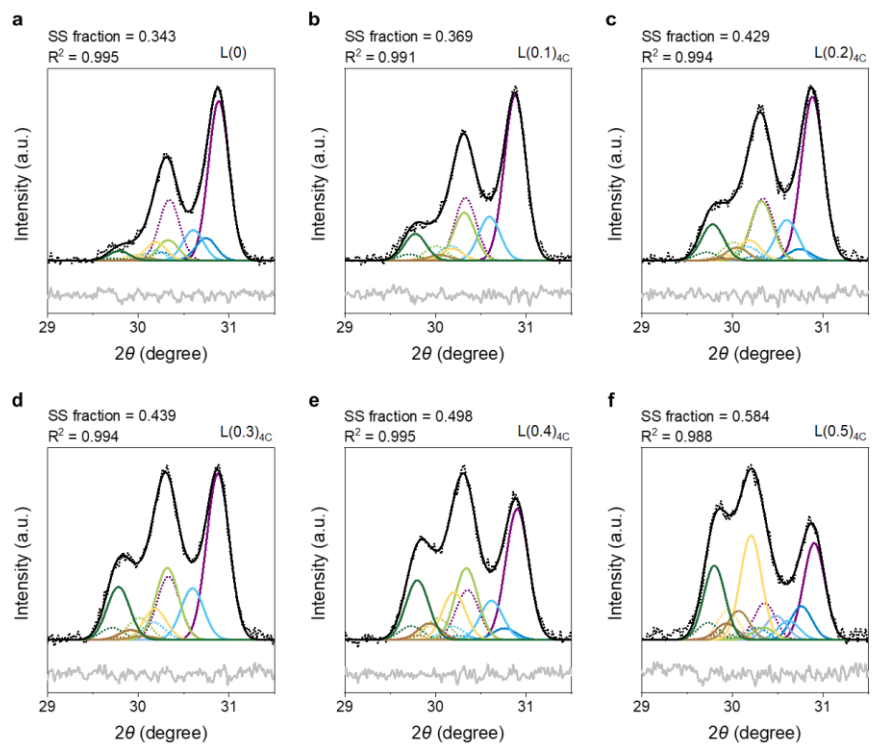
Supplementary Figure 2 XRD patterns of N(0.7)_{0.1C} hosts right after Na-ion insertion and after storage in N₂/H₂O glovebox (< 1 ppm O₂) for one month.



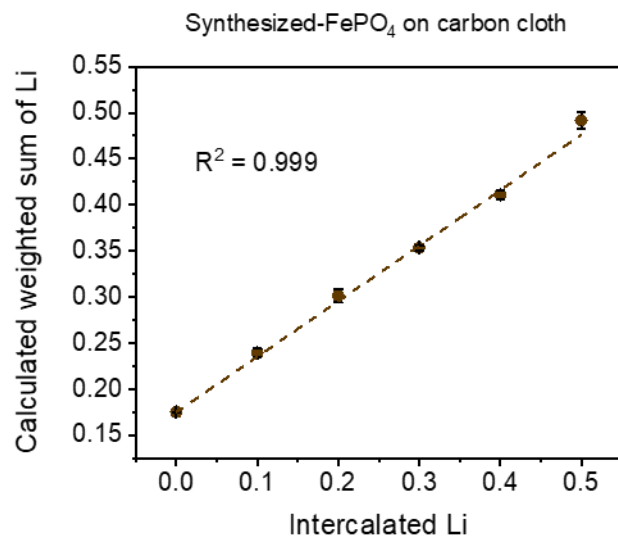
Supplementary Figure 3 XRD patterns of synthesized LiFePO_4 microplatelets and Li-Na co-intercalated $\text{LN}(0.7)_{0.1\text{C}}$ microplatelets. Green dashed lines denote the characteristic peaks of olivine LiFePO_4 phase (01-077-8344), and orange dashed lines denote the characteristic peaks of olivine $\text{Na}_{0.71}\text{FePO}_4$ intermediate phase (01-079-6974).



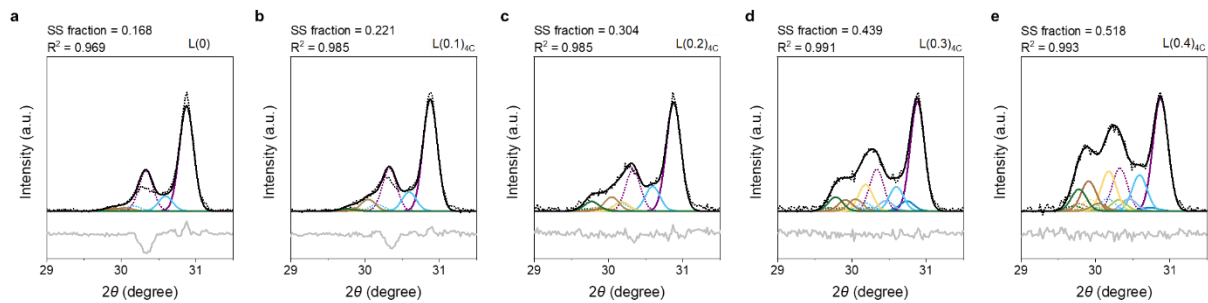
Supplementary Figure 4 Le Bail refinement of (a) Synthesized LiFePO_4 and (b) Chemically Li-extracted FePO_4 .



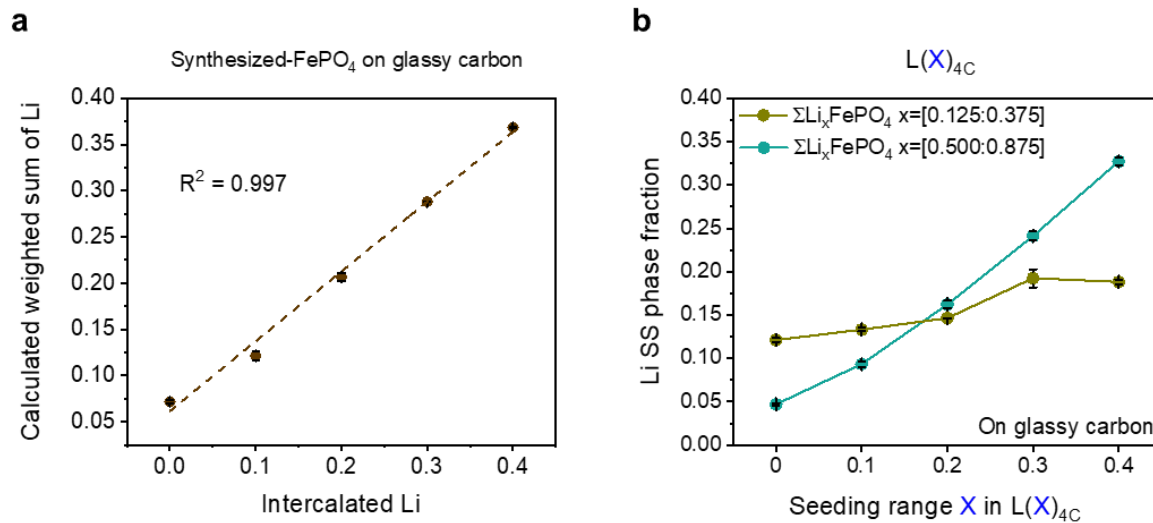
Supplementary Figure 5 Deconvoluted XRD patterns of (a) Chemically Li-extracted FePO₄ before seeding L(0), (b) L(0.1)_{4C}, (c) L(0.2)_{4C}, (d) L(0.3)_{4C}, (e) L(0.4)_{4C} and (f) L(0.5)_{4C} for Synthesized-FePO₄ particles on carbon cloth substrate from one representative sample.



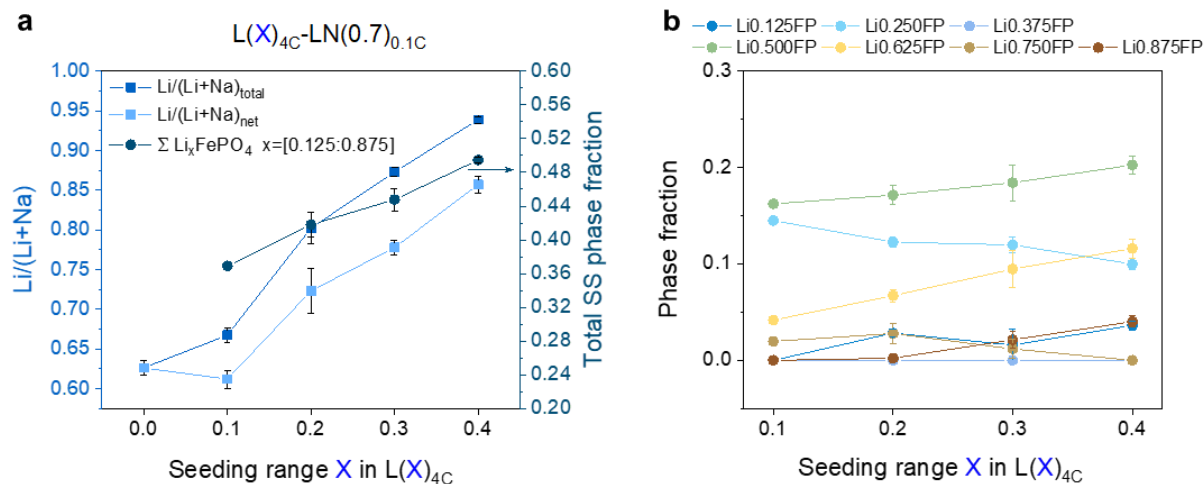
Supplementary Figure 6 Calculated weighted sum of Li from XRD fittings versus the electrochemically intercalated Li amount with the use of Synthesized-FePO₄ particles on carbon cloth. (Error bars representing the standard deviation of three replicate measurements.)



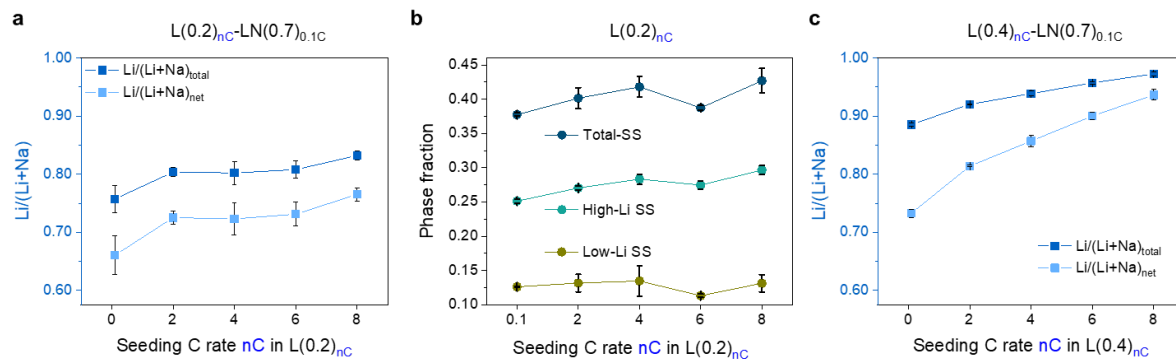
Supplementary Figure 7 Deconvoluted XRD patterns of (a) Chemically Li-extracted FePO_4 before seeding $\text{L}(0)$, (b) $\text{L}(0.1)_{4C}$, (c) $\text{L}(0.2)_{4C}$ (d) $\text{L}(0.3)_{4C}$, and (e) $\text{L}(0.4)_{4C}$ for Synthesized- FePO_4 particles on glassy carbon substrate from one representative sample.



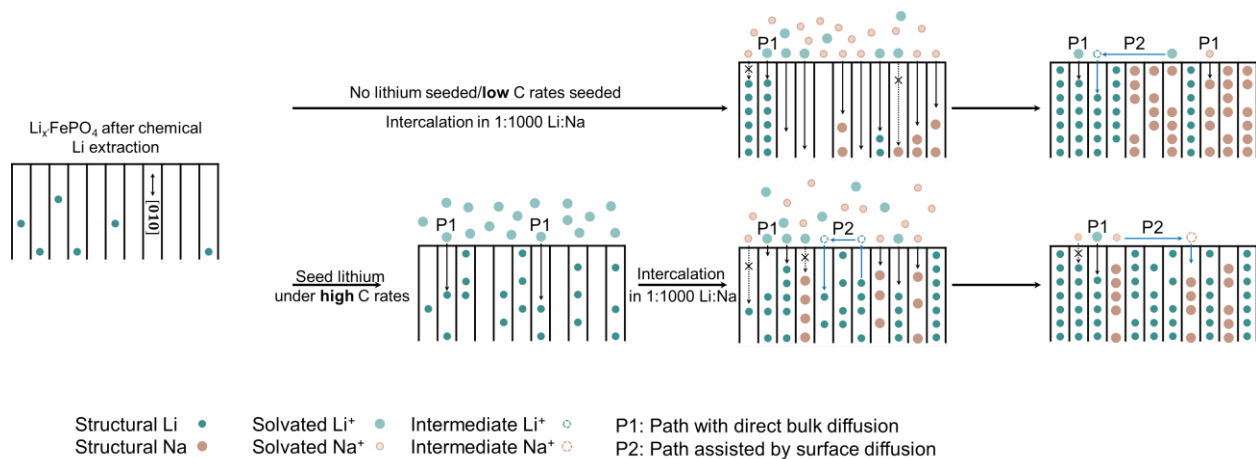
Supplementary Figure 8 (a) Calculated weighted sum of Li from XRD fittings versus the electrochemically intercalated Li ions amount with the use of Synthesized-FePO₄ particles on glassy carbon; (b) High-Li SS fractions (Li_xFePO₄, x = 0.500/0.625/0.750/0.875) and low-Li SS fractions (Li_xFePO₄, x = 0.125/0.250/0.375) under the same seeding rate 4C (588 mA/g) with different seeding ranges L(0/0.1/0.2/0.3/0.4)_{4C} collected on glassy carbon. (Error bars representing the standard deviation of three replicate measurements.)



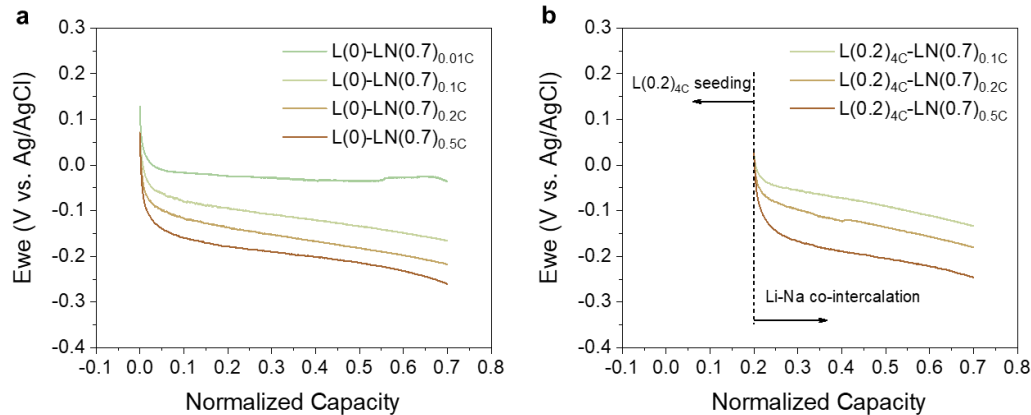
Supplementary Figure 9 (a) Total-SS fractions under the same seeding rate 4C (588 mA/g) with different seeding ranges $L(0/0.1/0.2/0.3/0.4)_{4C}$ and measured $Li/(Li+Na)_{total}$ and $Li/(Li+Na)_{net}$ ratios after 0.1C (14.7 mA/g) co-intercalation $L(X)_{4C}-LN(0.7)_{0.1C}$. (b) Individual phase fractions under the same seeding rate 4C (588 mA/g) with different seeding ranges $L(0/0.1/0.2/0.3/0.4)_{4C}$.



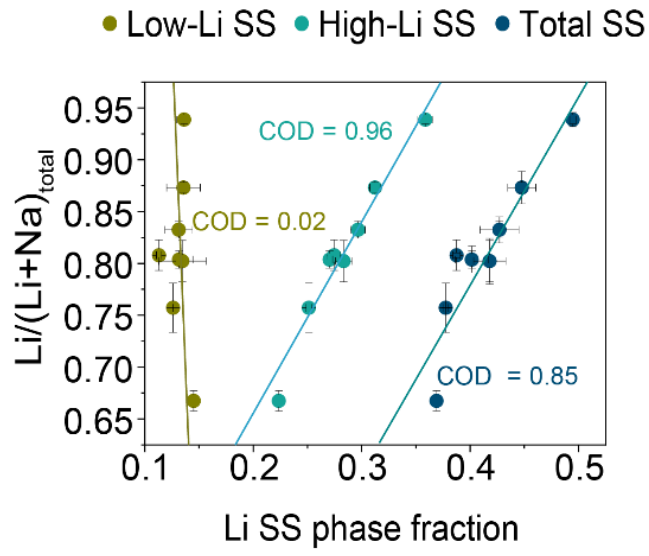
Supplementary Figure 10 (a) Recovered $Li/(Li+Na)_{total}$ and $Li/(Li+Na)_{net}$ of $L(0.2)_{0.1/2/4/6/8C}-LN(0.7)_{0.1C}$. (b) SS fractions under different seeding C rates with the same 20% seeding range $L(0.2)_{0.1/2/4/6/8C}$. (c) Recovered $Li/(Li+Na)_{total}$ and $Li/(Li+Na)_{net}$ of $L(0.4)_{0.1/2/4/6/8C}-LN(0.7)_{0.1C}$. (Noting that 1C is equivalent to 147 mA/g)



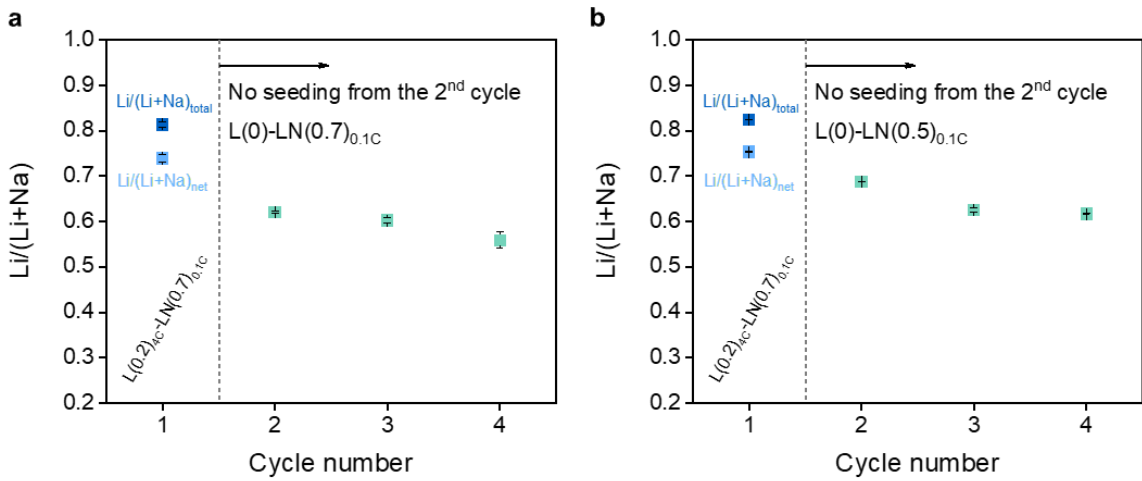
Supplementary Figure 11 Schematic illustration of Li-Na co-intercalation pathways for chemically Li extracted Li_xFePO₄ hosts (x' denotes the remnant quantity of Li in the structure due to the defect), low-rate Li pre-seeded hosts, and high-rate Li pre-seeded hosts.



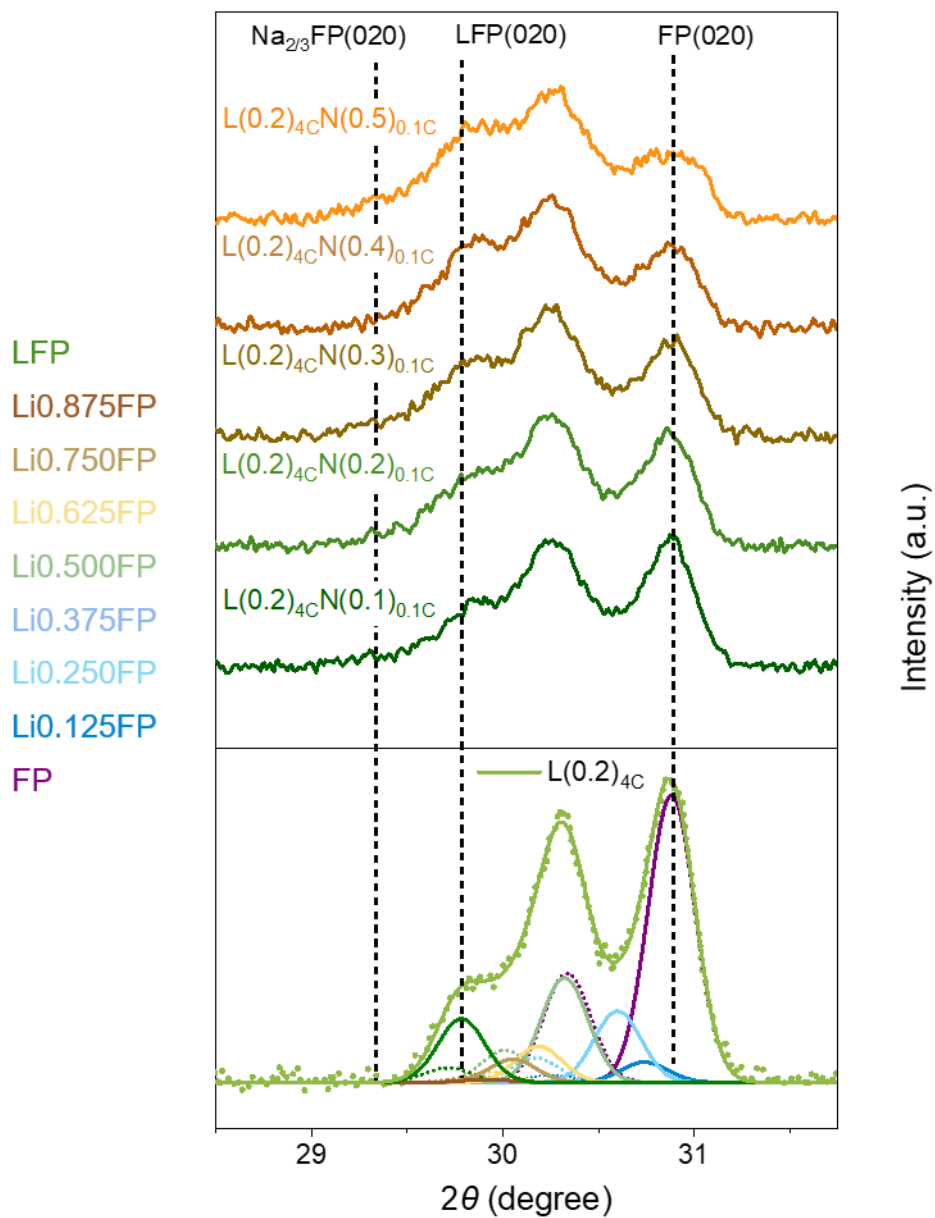
Supplementary Figure 12 Intercalation curves of (a) $L(0)$ -LN(0.7)_{0.01/0.1/0.2/0.5C and (b) $L(0.2)_{4C}$ -LN(0.7)_{0.1/0.2/0.5C}.} Without (L(0)) or with 4C (588 mA/g) Li seeding ($L(0.2)_{4C}$), all the working electrodes, paired with NaFePO_4 counter electrodes and $\text{Ag}|\text{AgCl}|\text{KCl}$ (4.0 M) reference electrodes, would undergo intercalation in a three-neck round-bottomed flask containing 500 mL synthetic brine solutions (1 mM LiCl and 1 M NaCl mixed solution) at room temperature (20 ~ 25 °C). Different intercalation C rates (0.01C, 0.1C, 0.2C, or 0.5C; 0.1C equals to 14.7 mA/g) were used until 70% of the total capacity. N_2 (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O_2 .



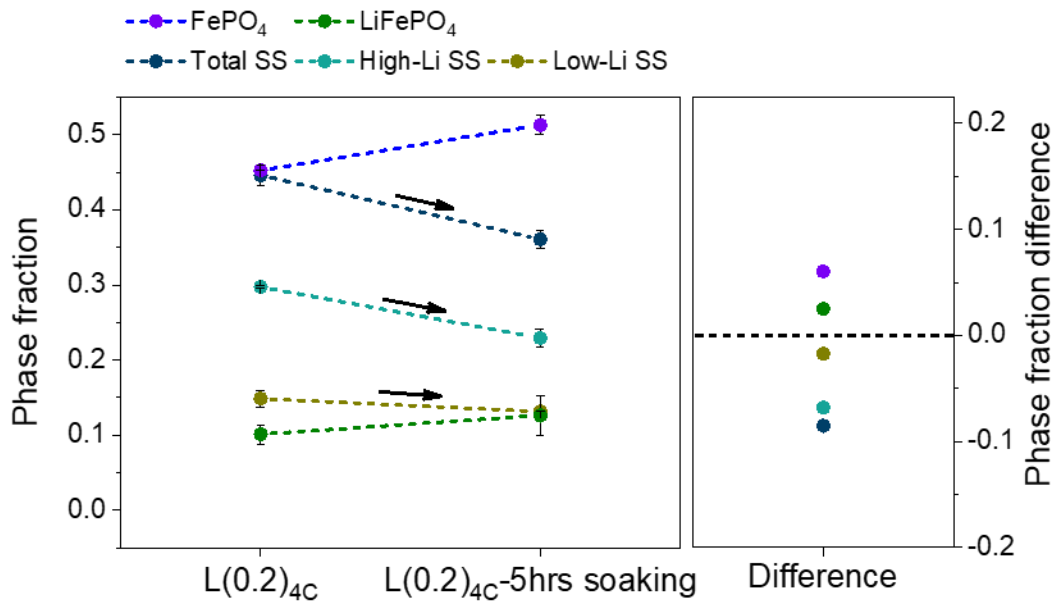
Supplementary Figure 13 $\text{Li}/(\text{Li}+\text{Na})_{\text{total}}$ vs. low-Li/high-Li/total-Li SS fractions and corresponding coefficients of determination (COD). (Error bars representing the standard deviation of three replicate measurements)



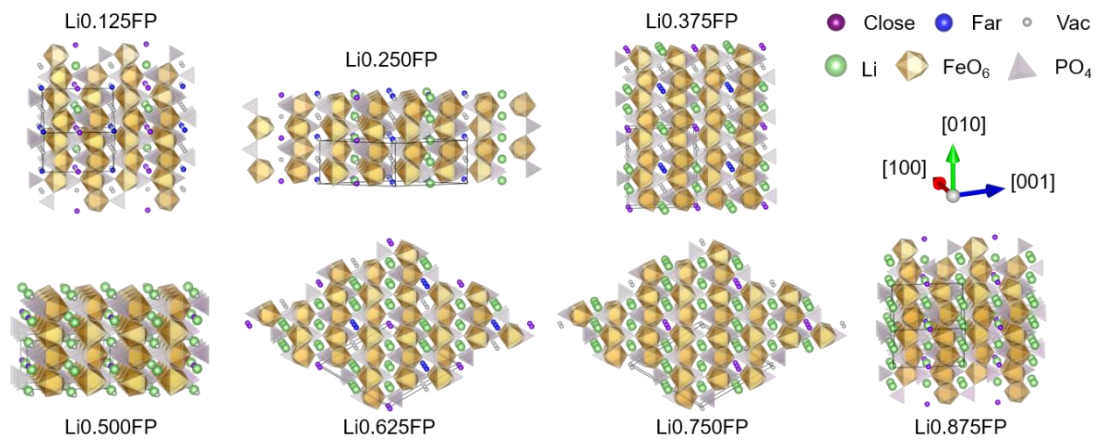
Supplementary Figure 14 $\text{Li}/(\text{Li}+\text{Na})_{\text{net}}$ for the multi-intercalation stability test using 20% Li seeding for the 1st cycle and skipping Li seeding for the following cycles. (a) 70% capacity usage from the 2nd cycle, L(0)-LN(0.7)_{0.1C}. (b) 50% capacity usage from the 2nd cycle, L(0)-LN(0.5)_{0.1C}.



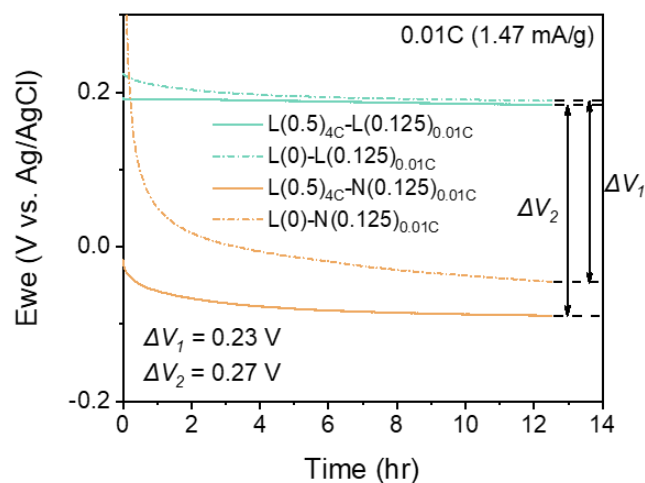
Supplementary Figure 15 Ex situ XRD evolution of $L(0.2)_{4C}$ preseeded host during Na insertion $L(0.2)_{4C}N(0/0.1/0.2/0.3/0.4/0.5)_{0.1C}$. Color texts denote the deconvoluted Li SS phases for $L(0.2)_{4C}$. (Dotted lines: raw data; Solid lines: fit)



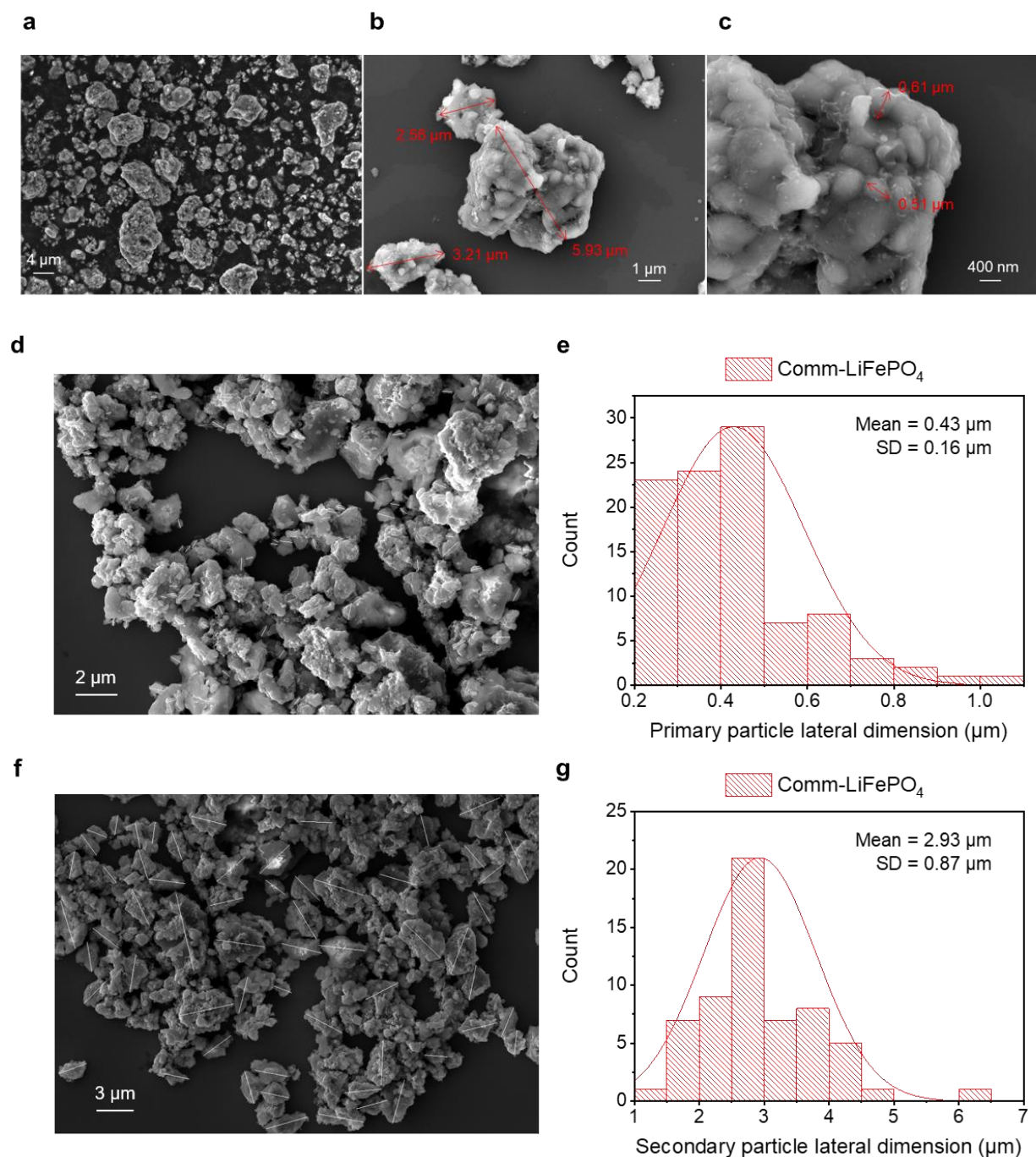
Supplementary Figure 16 Fitted phase fractions for L(0.2)_{4C} microplatelets before and after 5hrs soaking in 1M NaCl_(aq). (Error bars representing the standard deviation of three replicate measurements.)



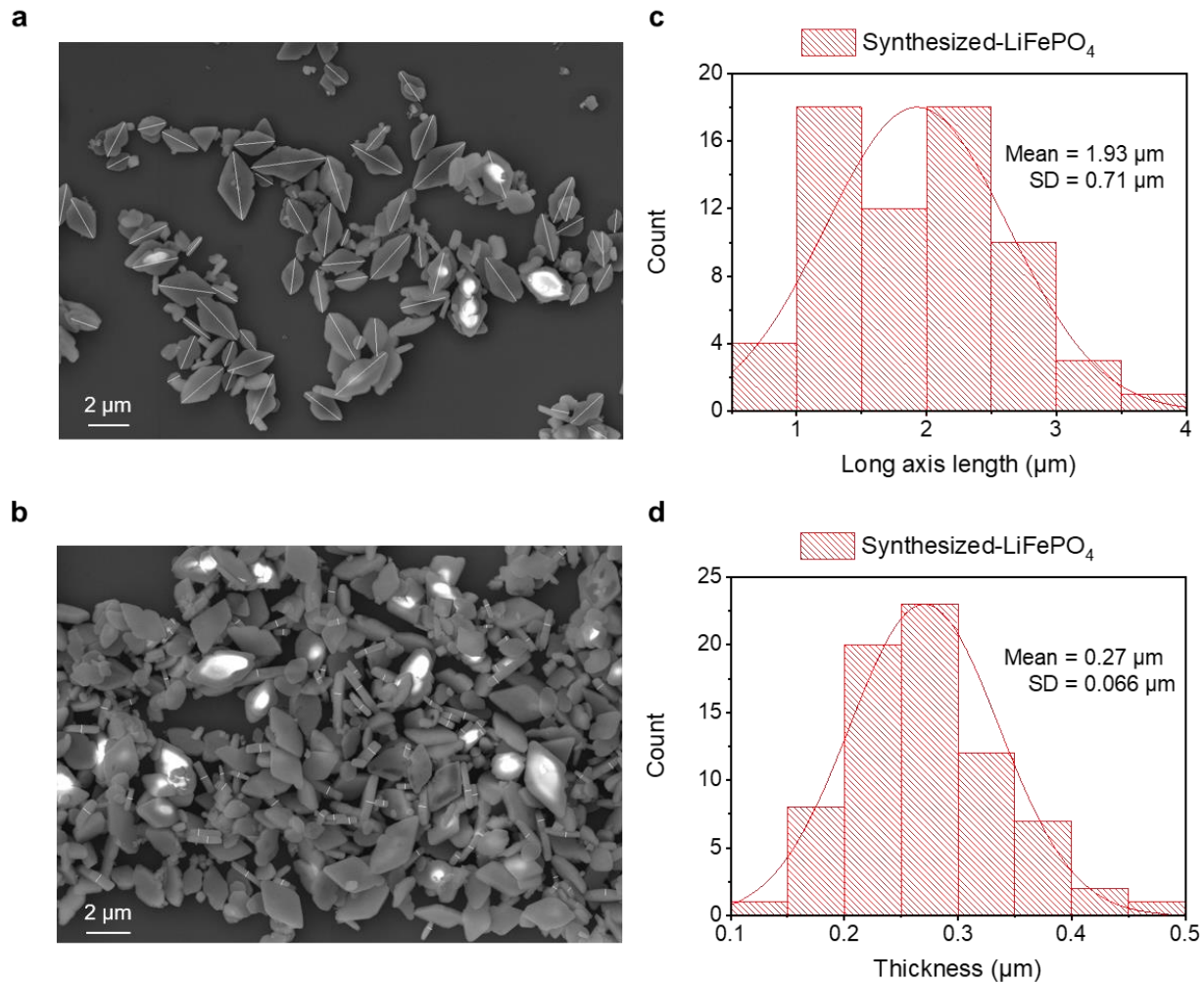
Supplementary Figure 17 Structures for the seven intermediate phases with either close or far intercalation positions labeled.



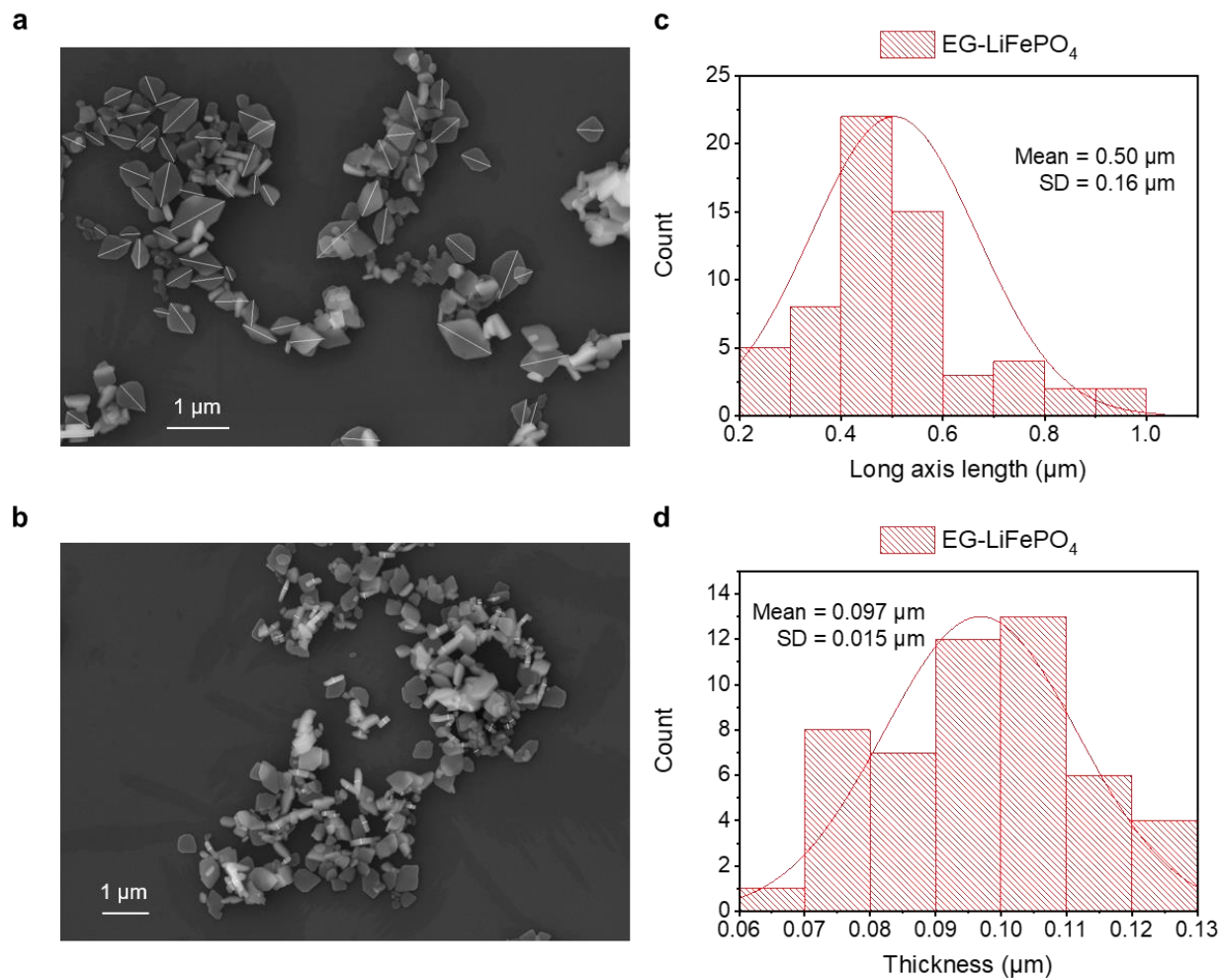
Supplementary Figure 18 Intercalation curves of chemically Li-extracted hosts (L(0); dash-dot lines) and 4C (588 mA/g) 50% Li pre-seeded hosts (L(0.5)_{4C}; solid lines) in 60 mL either 1 M LiCl (green) or 1 M NaCl (orange) aqueous solution until 12.5% of capacity are used under 0.01C (1.47 mA/g) at room temperature (20 ~ 25 °C). The reference electrode is always Ag|AgCl|KCl (4.0 M). To avoid co-intercalation, in 1 M LiCl aqueous solution, the counter electrode is LiFePO₄; while in 1 M NaCl aqueous solution, the counter electrode is NaFePO₄. N₂ (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O₂.



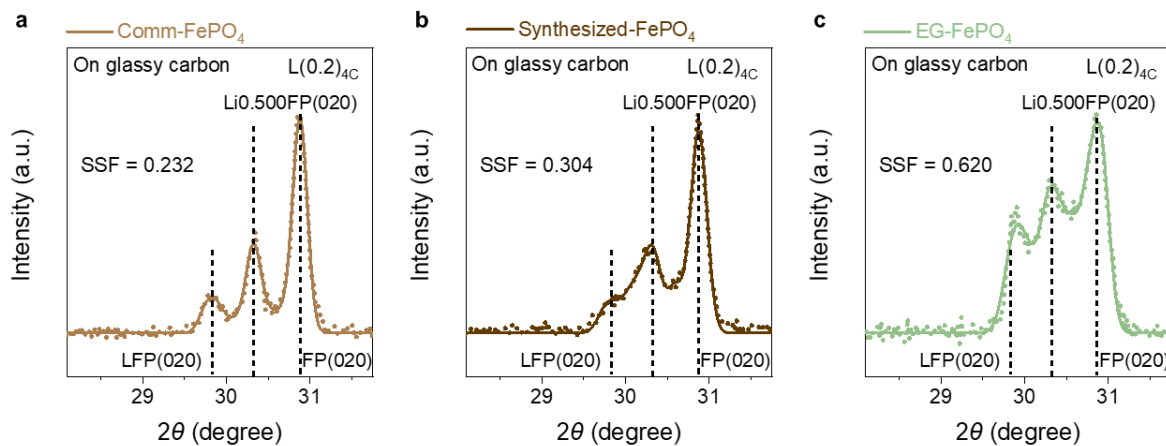
Supplementary Figure 19 SEM images for Comm-LiFePO₄ particles. (a) Comm-LiFePO₄ particles dropped on carbon tape, (b) Magnified SEM for Comm-LiFePO₄ secondary particles dispersed on Si wafer, (c) Magnified SEM for Comm-LiFePO₄ primary particles on Si, additional SEM images and corresponding lateral distribution summary of primary (d, e) and secondary (f, g) Comm-LiFePO₄ particles dispersed on Si wafer. (Only the isolated and fully exposed particles were counted; the thin white lines in the SEM images denoted the measured length.)



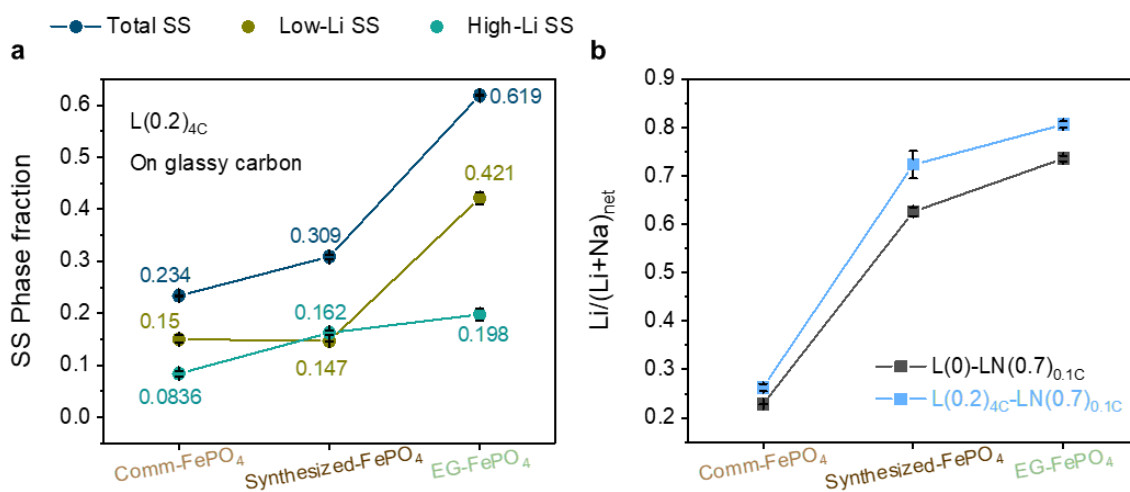
Supplementary Figure 20 SEM images of Synthesized-LiFePO₄ particles (a, b) with corresponding particle dimension distribution along the long axis (c) or thickness (d). (Only the isolated and fully exposed particles were counted; the thin white lines in the SEM images denoted the measured length.)



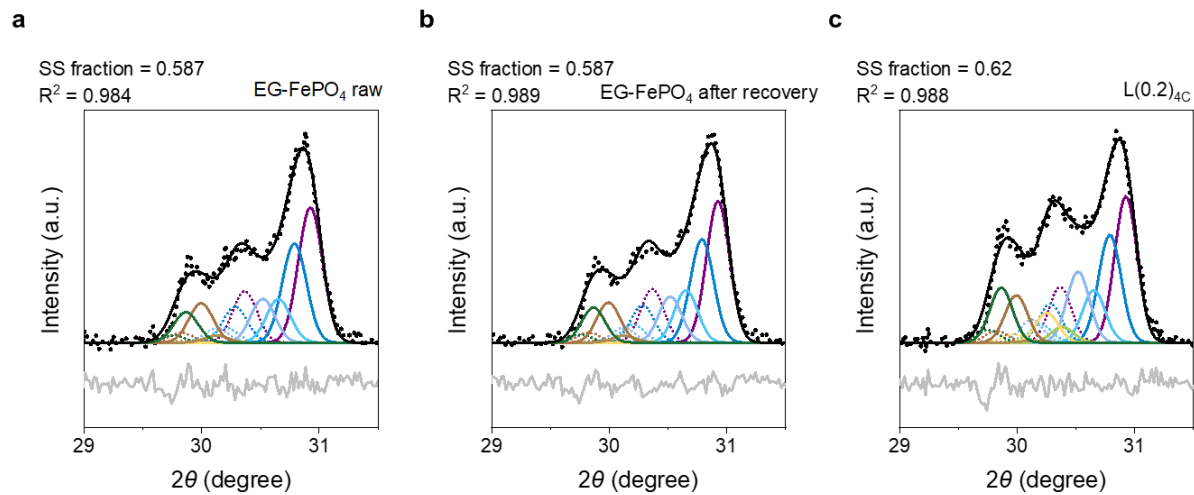
Supplementary Figure 21 SEM images of EG-LiFePO₄ particles (a, b) with corresponding particle dimension distribution along the long axis (c) or thickness (d). (Only the isolated and fully exposed particles were counted; the thin white lines in the SEM images denoted the measured length.)



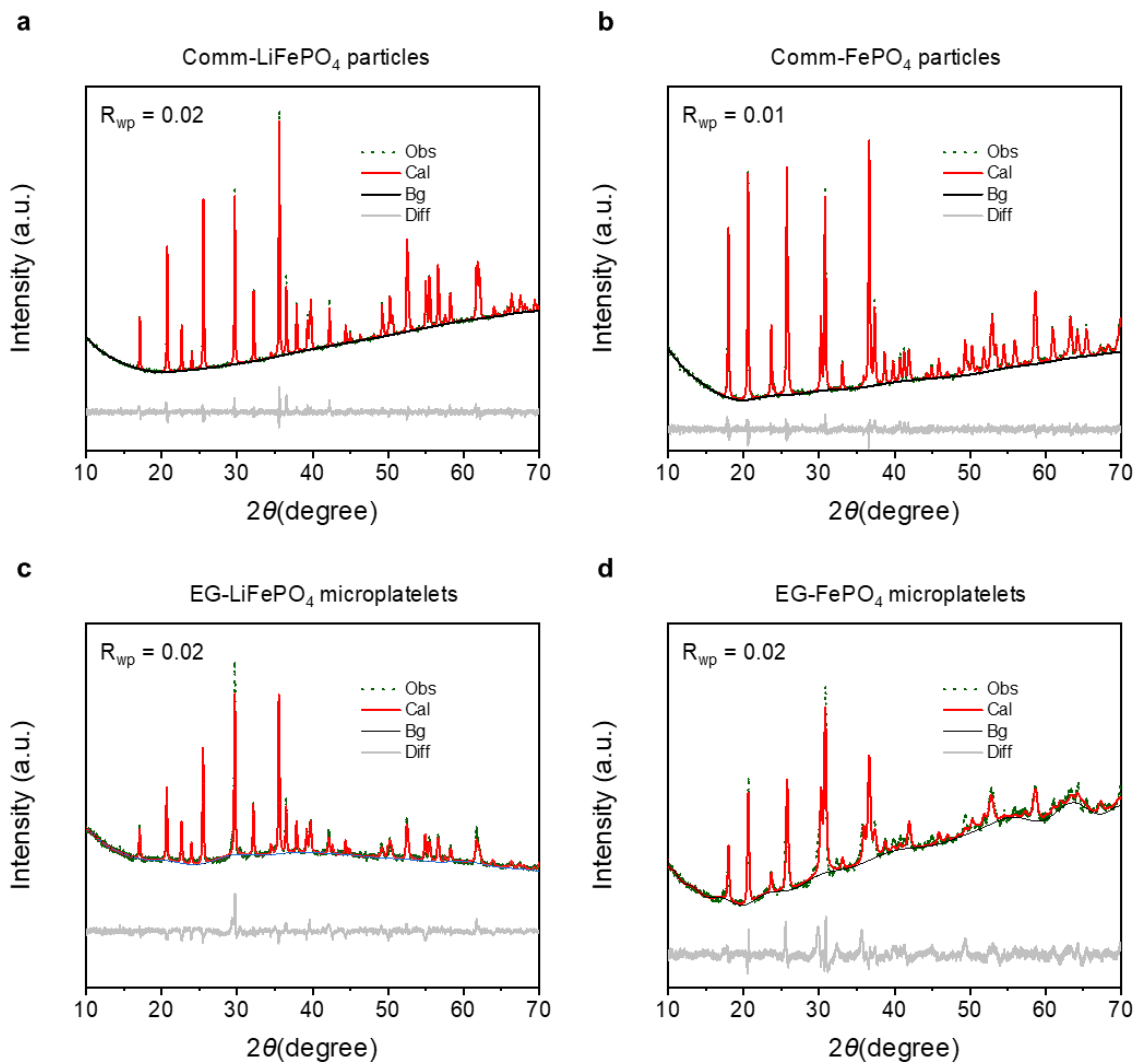
Supplementary Figure 22 Example XRD patterns of (a) Comm-FePO₄, (b) Synthesized-FePO₄, and (c) EG-FePO₄ electrodes after 20% of Li seeding under 4C collected on glassy carbon. For Comm-FePO₄, 135 mA/g equals a rate of 1C; for Synthesized-FePO₄, 147 mA/g equals a rate of 1C; for EG-FePO₄, 125 mA/g equals a rate of 1C (Dotted lines: raw data; Solid lines: fit).



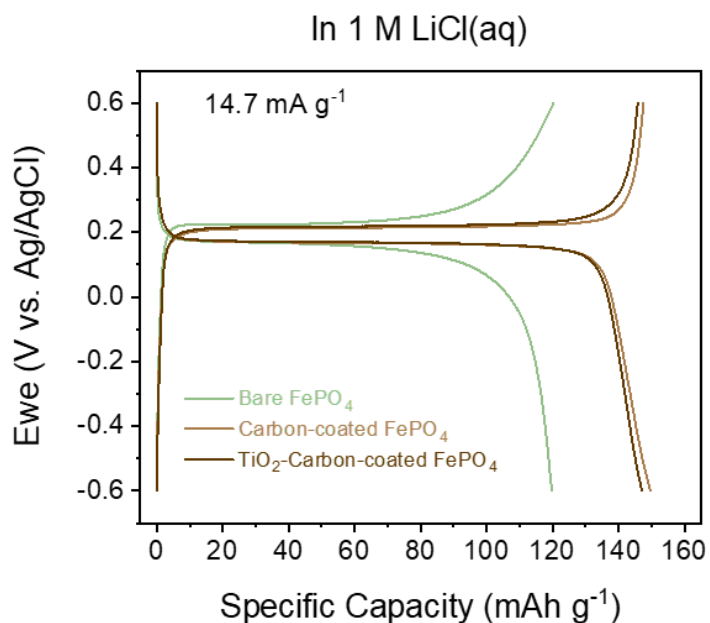
Supplementary Figure 23 (a) Total SS, Low-Li SS, and High-Li SS fractions for the three different FePO₄ samples under the same seeding rate 4C (540 mA/g for Comm-FePO₄; 588 mA/g for Synthesized-FePO₄; 500 mA/g for EG-FePO₄) with the 20% seeding range L(0.2)_{4C}. **(b)** Recovered Li/(Li+Na)_{net} of the three electrodes until 70% of the total capacity used under 0.1C, with either initial 20% of Li seeding under 4C (L(0.2)_{4C}-LN(0.7)_{0.1C}) or without any initial seeding process (L(0)-LN(0.7)_{0.1C}). (Error bars represent the standard deviation of three replicate measurements.)



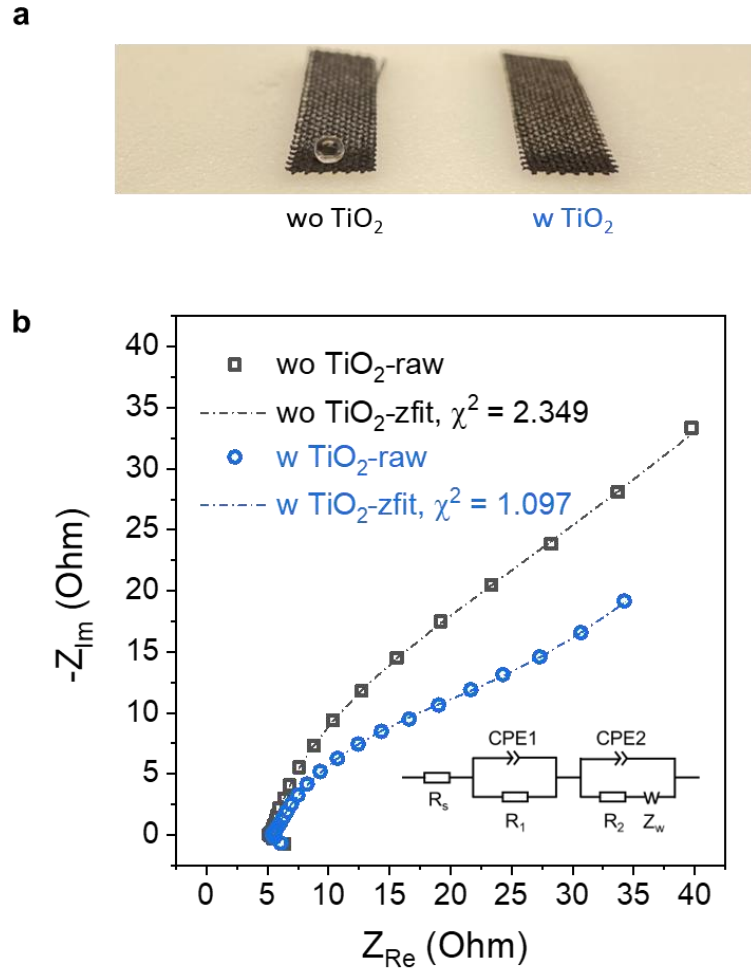
Supplementary Figure 24 Deconvoluted XRD patterns of EG-FePO₄ on glassy carbon (a) raw electrodes, (b) after Li recovery, and (c) After 4C 20% Li seeding, L(0.2)_{4C}. (Dotted lines: raw data; Solid lines: fit).



Supplementary Figure 25 Leball refinement of (a) Comm-LiFePO₄ particles, (b) chemical-extracted Comm-LiFePO₄ particles, (c) EG-LiFePO₄ particles, and (d) chemical-extracted EG-FePO₄ particles.



Supplementary Figure 26 Electrochemical cycling of Bare, Carbon-coated and TiO₂-Carbon-coated FePO₄ electrodes in 60 mL 1 M LiCl aqueous solution between -0.6 V and 0.6 V (vs. Ag/AgCl/KCl (4.0 M)) at room temperature (20 ~ 25 °C) under 0.1C (14.7 mA/g). 147 mA/g equals a rate of 1C. The counter electrode is LiFePO₄. N₂ (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O₂.



Supplementary Figure 27 (a) Photographic image showing 10 μL water dropped on the surface of the carbon-coated FePO_4 electrode wo/w 3nm TiO_2 coating. (b) Nyquist plots for the electrode wo/w 3nm TiO_2 obtained by electrochemical impedance spectroscopy (EIS) tests in 1 M LiCl aqueous solution with the frequency ranging from 200 kHz to 100 mHz at a 10 mV amplitude. The dot-dashed lines are the fitting curves by using the equivalent circuit, which is shown as the inset and consists of a resistor (R_s), a resistor (R_1) paralleled with a constant phase element (CPE), and a CPE parallel with a resistor (R_2) which is connected with a Warburg element (Z_w) in series.

(Noting that χ^2 gives an estimation of the distance between the real data and the simulated data. Its

$$\text{expression is: } \chi^2 = \sum_{i=1}^n \frac{|Z_{measured}(i) - Z_{simulated}(f_i, param)|^2}{\sigma_i^2}$$

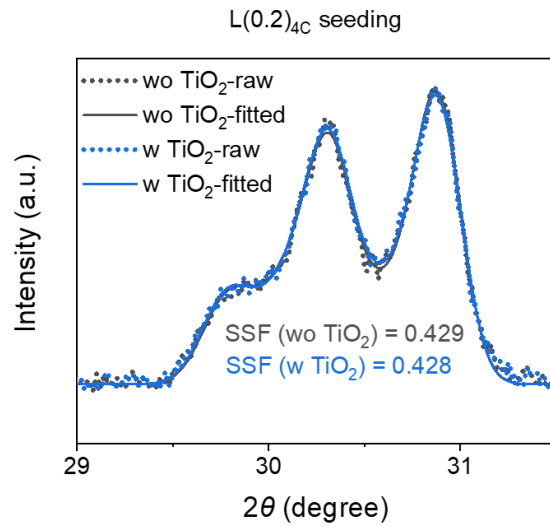
with $Z_{measured}(i)$ is the measured impedance at the f_i frequency;

$Z_{simulated}(f_i, param)$ is a function of the chosen model;

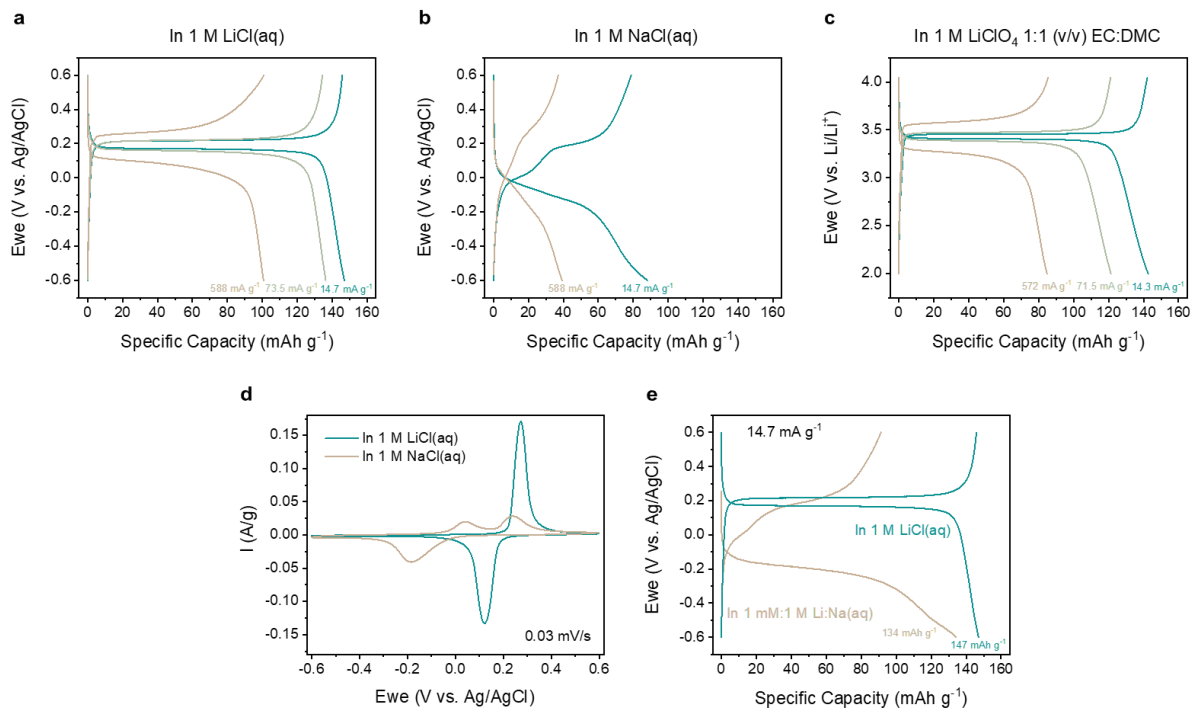
f_i is the frequency i ;

$param$ is the model parameters (ex: R_1 , R_2 , C_1 , Q_1 , ...);

σ_i is the standard deviation)

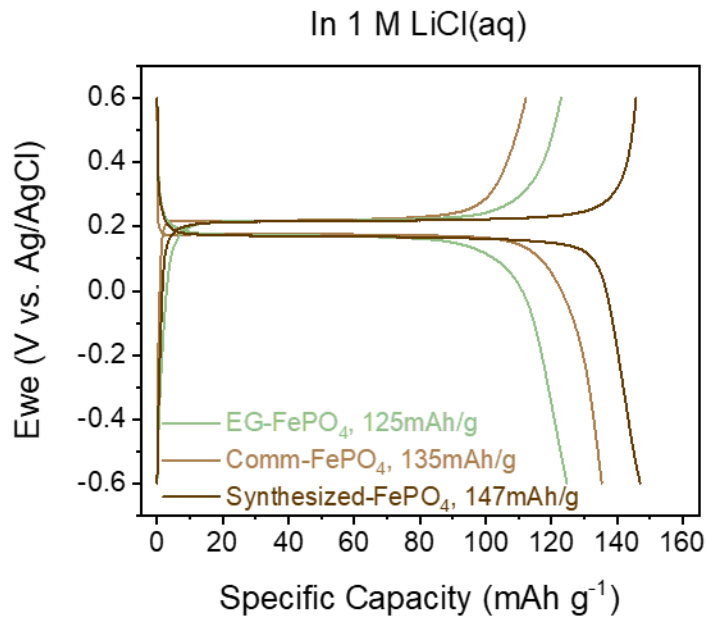


Supplementary Figure 28 XRD of the carbon-coated FePO₄ electrode wo/w 3nm TiO₂ coating after 20% Li seeding under 4C (588 mA/g) (Dotted lines: raw data; Solid lines: fit).

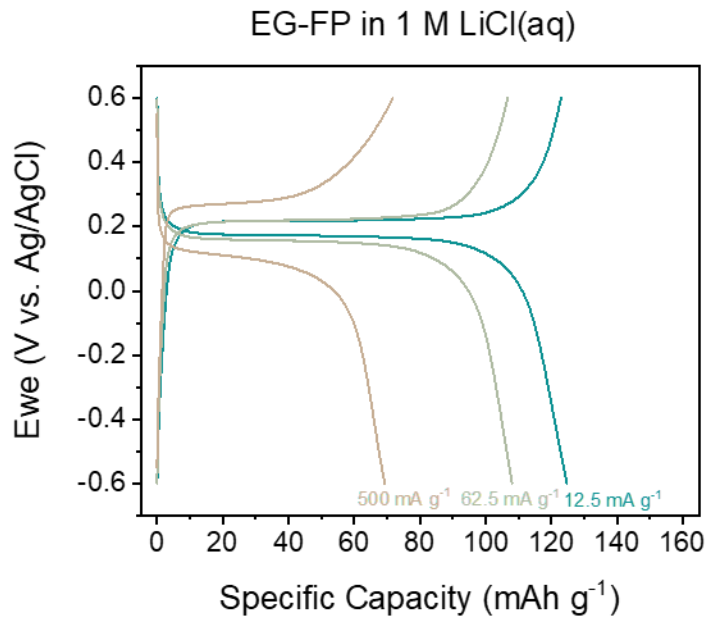


Supplementary Figure 29 Electrochemical energy storage performance of Synthesized-FePO₄ in aqueous electrolyte solution. Electrochemical cycling of the Synthesized-FePO₄ electrodes in (a) 60 mL 1 M LiCl aqueous solution (paired with Ag/AgCl/KCl (4.0 M) reference and LiFePO₄ counter electrodes) and (b) 60 mL 1 M NaCl aqueous solution (paired with Ag/AgCl/KCl (4.0 M) reference and NaFePO₄ counter electrodes) under different specific currents/C rates. 14.7 mA/g equals a rate of 0.1C, while 147 mA/g equals 1C. (c) Electrochemical cycling of the Synthesized-FePO₄ electrodes in 60 mL 1 M LiClO₄ 1:1 (v/v) ethylene carbonate and dimethyl carbonate electrolyte under different specific currents/C rates (paired with Ag/AgCl/(0.1M tetrabutylammonium perchlorate + 0.01M AgNO₃ in acetonitrile) reference and LiFePO₄ counter electrodes). 143 mA/g equals a rate of 1C in the organic setup. (d) Cyclic voltammetry (CV) tests for the Synthesized-FePO₄ electrodes in 60 mL 1 M LiCl/NaCl aqueous solution at a 0.03 mV/s scan rate (paired with Ag/AgCl/KCl (4.0 M) reference and LiFePO₄/NaFePO₄ counter electrodes). (e) Comparison of electrochemical cycling of the Synthesized-FePO₄ electrodes in 60 mL 1 M LiCl and 500 mL 1 mM LiCl: 1 M NaCl aqueous solutions under 0.1C (14.7 mA/g), using Ag/AgCl/KCl (4.0 M) and LiFePO₄/NaFePO₄ as the reference and counter electrodes.

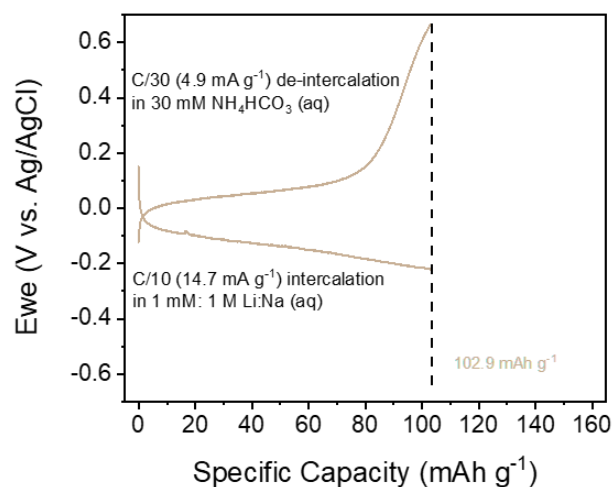
(Noting that all the electrochemical operations were performed at room temperature (20 ~ 25 °C) with N₂ (purity > 99.998%) continuously bubbled into the solution from the inlet. Specifically, no climatic/environmental chamber is used.)



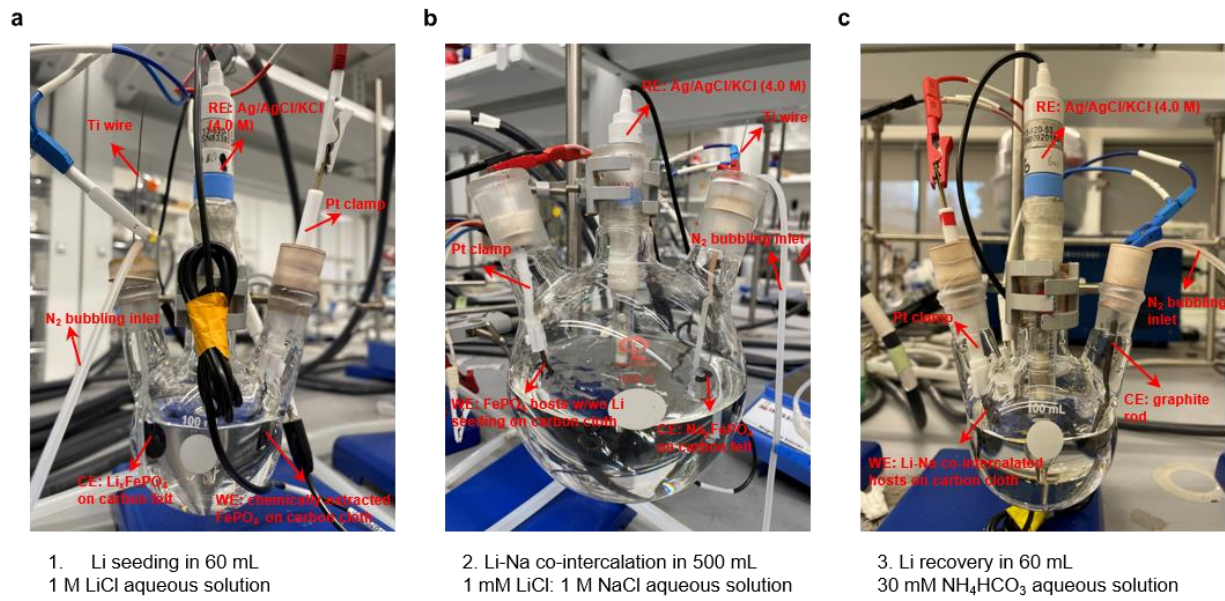
Supplementary Figure 30 Electrochemical cycling of Comm-FePO₄ (13.5 mA/g), Synthesized-FePO₄ (14.7 mA/g), and EG-FePO₄ (12.5 mA/g) electrodes in 60 mL 1 M LiCl aqueous solutions between -0.6 V and 0.6 V (vs. Ag/AgCl/KCl (4.0 M)) at room temperature (20 ~ 25 °C). The counter electrode is LiFePO₄. N₂ (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O₂.



Supplementary Figure 31 Electrochemical cycling of EG-FePO₄ particles in 60 mL 1 M LiCl aqueous solution and under different specific currents/C rates at room temperature (20 ~ 25 °C) under 0.1C (12.5 mA/g). 125 mA/g equals a rate of 1C for EG-FePO₄. The counter electrode is LiFePO₄. The reference electrode is Ag|AgCl|KCl (4.0 M). N₂ (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O₂.



Supplementary Figure 32 One example electrochemical extraction cycle. 0.1C (14.7 mA/g) intercalation curve in 500 mL 1 mM LiCl: 1 M NaCl aqueous solution and C/30 (4.9 mA/g) de-intercalation curve in 60 mL 30 mM NH₄HCO₃ recovery solution, with the use of 70% of the total capacity (102.9 mAh/g). For both intercalation and de-intercalation, N₂ (purity > 99.998%) was continuously bubbled into the solution to avoid side reactions caused from dissolved O₂, and the reference electrode is Ag|AgCl|KCl (4.0 M) with the testing temperature at room temperature (20 ~ 25 °C). NaFePO₄ was used as the counter electrode during the intercalation process; while graphite rod was used as the counter electrode during the de-intercalation process.



Supplementary Figure 33 Detailed images of the cells used during (a) Li seeding, (b) Li-Na co-intercalation, and (c) Li recovery processes. (CE: counter electrode; RE: reference electrode; WE: working electrode)

Supplementary Table 1 Lattice parameters for potentially related Li or Na phases and the normalized values by the value of olivine FePO₄ (00-065-0258) phase. Lattice parameters of olivine FePO₄ are set as one.

	b [010] (Å)	a [100] (Å)	c [001] (Å)	α	β	γ	Volume (Å ³)	c/a	a/b	c/b
Olivine LFP (01-077-8344)	6.009 (+ 3.7%)	10.329 (+ 5.2%)	4.695 (- 1.9%)	90.00°	90.00°	90.00°	291.38 (+ 7%)	0.781	0.582	0.455
Olivine N _{2/3} FP (01-079-6974)	6.082 (+ 5.0%)	10.289 (+ 4.8%)	4.937 (+ 3.1%)	90.00°	90.00°	90.00°	308.96 (+ 13%)	0.812	0.591	0.480
Olivine NFP (01-079-6973)	6.219 (+ 7.3%)	10.406 (+ 6.0%)	4.947 (+ 3.3%)	90.00°	90.00°	90.00°	320.13 (+ 18%)	0.795	0.598	0.475
Olivine FP (00-065-0258)	5.795 (1.0)	9.821 (1.0)	4.787 (1.0)	90.00°	90.00°	90.00°	272.46 (1.0)	0.826	0.590	0.487
Maricite NFP (01-071-5040)	6.874 (+ 18.8%)	9.001 (- 8.4%)	5.052 (+ 5.5%)	90.00°	90.00°	90.00°	312.58 (+ 15%)	0.735	0.764	0.561

Supplementary Table 2 Lattice parameters for all the phases.

	LFP	L0.875FP	L0.750FP	L0.625FP	L0.500FP	L0.375FP	L0.250FP	L0.125FP	FP
a	10.347	10.281	10.215	10.149	10.083	10.017	9.951	9.885	9.819
b	6.007	5.981	5.955	5.929	5.903	5.877	5.850	5.824	5.798
c	4.700	4.711	4.721	4.732	4.743	4.753	4.764	4.775	4.785
α	90								
β									
γ									

Supplementary Table 3 (211) and (020) peak positions for all the phases.

Peak	LFP	L0.875FP	L0.750FP	L0.625FP	L0.500FP	L0.375FP	L0.250FP	L0.125FP	FP
(211)	29.69	29.76	29.83	29.91	29.98	30.06	30.14	30.23	30.31
(020)	29.76	29.89	30.02	30.16	30.30	30.43	30.57	30.71	30.86

Supplementary Table 4 (211) and (020) area ratios for all the phases.

Area ratio	LFP	L0.875FP	L0.750FP	L0.625FP	L0.5FP	L0.375FP	L0.25FP	L0.125FP	FP
$\frac{(211)}{(020)}$	0.23	0.249	0.268	0.286	0.305	0.324	0.343	0.361	0.38

Supplementary Table 5 Fitted phase fractions of Supplementary Figure 5 with the calculated weighted sum of Li.

	LFP	L0.875FP	L0.75FP	L0.625FP	L0.5FP	L0.375FP	L0.25FP	L0.125FP	FP	Intercalated Li	Weighted sum of Li
L(0)	0.04559	0	0.00688	0.07342	0.0824	0	0.11461	0.06579	0.61132	0	0.17471
L(0.1) _{4C}	0.07562	0	0.01964	0.04159	0.16232	0	0.14505	0	0.55578	0.1	0.23377
L(0.2) _{4C}	0.11218	0.00506	0.03933	0.06099	0.17481	0	0.11613	0.03272	0.45878	0.2	0.30475
L(0.3) _{4C}	0.14591	0.02684	0.01063	0.08277	0.18803	0	0.13107	0	0.41474	0.3	0.35589
L(0.4) _{4C}	0.16798	0.04583	0	0.12913	0.19123	0	0.10210	0.02974	0.33398	0.4	0.41365
L(0.5) _{4C}	0.19104	0.04145	0.07255	0.25751	0.02989	0.05795	0.04552	0.07888	0.2252	0.5	0.50058

Supplementary Table 6 Fitted phase fractions of Supplementary Figure 7 with the calculated weighted sum of Li.

	LFP	L0.875FP	L0.75FP	L0.625FP	L0.5FP	L0.375FP	L0.25FP	L0.125FP	FP	Low-Li SS	High-Li SS	Intercalated Li	Weighted sum of Li
L(0)	0	0.02175	0.02672	0	0	0	0.1191	0	0.83166	0.1191	0.04847	0	0.06962
L(0.1) _{4C}	0.01511	0.00562	0.08468	0	0	0	0.13104	0	0.76355	0.13104	0.0903	0.1	0.1163
L(0.2) _{4C}	0.06107	0.01466	0.08725	0.05607	0	0	0.14645	0	0.63449	0.14645	0.15798	0.2	0.21099
L(0.3) _{4C}	0.06909	0.05342	0.05712	0.12553	0	0.04728	0.11082	0.04485	0.49188	0.20295	0.23607	0.3	0.28817
L(0.4) _{4C}	0.08447	0.11453	0.02793	0.14864	0.04111	0.04378	0.12912	0.01258	0.39784	0.18548	0.33221	0.4	0.36936

Supplementary Table 7 Li selectivity over Na with FePO₄ in the literature and this work. (*: 46.4 mg Li/g FePO₄ is equivalent to 170 mAh/g capacity used)

Reference	Specific current during extraction (mA/g)	Capacity used during extraction (mAh/g)	Initial Li:Na (at%)	Recovered Li:Na (at%)	Selectivity
LiFePO ₄ ¹	22.2	44.4	50 mM:5 M (1:100)	5.7:1	5.70 × 10 ²
		44.4	5 mM:5 M (1:1000)	1:1.8	5.60 × 10 ²
		44.4	0.5 mM:5 M (1:10000)	1:4.0	2.50 × 10 ²
LiFePO ₄ ²	62.5	62.5	0.1 M:0.1 M (1:1)	225.0:1	2.25 × 10 ²
		62.5	1 M:1 M (1:1)	17250.0:1	1.73 × 10 ⁴
	6.25	62.5	42 mM:793 mM (1:19; Atacama)	9250.0:1	1.76 × 10 ⁵
	62.5	62.5		106.5:1	2.02 × 10 ³
	625	62.5		3.1:1	59
LiFePO ₄ ³	0.184	0.66 (~215 mins operation)	5 mM:0.5 M (1:100)	2.6:1 (dissolved solid)	2.60 × 10 ²
LiFePO ₄ w/ Polydopamine coating ³		0.66 (~215 mins operation)		43.3:1 (dissolved solid)	4.33 × 10 ³
LiFePO ₄ ⁴	Chemical reaction, using potassium persulfate as the oxidant	*45.3 mg Li/g FePO ₄	60 mM:6 M (1:100)	39.2:1 (dissolved solid)	3.92 × 10 ³
		*44.8 mg Li/g FePO ₄	60 mM:3 M (1:50)	49.1:1 (dissolved solid)	2.46 × 10 ³
		*35.1 mg Li/g FePO ₄	60 mM:0.6 M (1:10)	38.4:1 (dissolved solid)	3.84 × 10 ²
		*45.7 mg Li/g FePO ₄	60 mM:4.6 M (1:77)	61.0:1 (dissolved solid)	4.70 × 10 ³
		*46.4 mg Li/g FePO ₄	200 mM:3 M (1:15)	370.0:1 (dissolved solid)	5.55 × 10 ³
LiFePO ₄ w/ TiO ₂ coating ⁵	34	51	0.025 mM:0.47 M (1:18500, Seawater)	1:2.18	8.49 × 10 ³
	17 (P _{10s} - equivalent specific current)	51	0.025 mM:0.47 M (1:18500, Seawater)	1:1.01	1.83 × 10 ⁴
	17 (P _{1s} - equivalent specific current)	51	0.025 mM:0.47 M (1:18500, Seawater)	1:1.11	1.67 × 10 ⁴
	10.625	53.125	0.025 mM:0.47 M	1.01:1	1.87 × 10 ⁴

	(P _{10s} R _{2s} - equivalent specific current)			(1:18500, Seawater)		
	17 (P _{10s} - equivalent specific current)	51		0.025 mM:0.47 M (1:18500, Li-Na binary)	1:1	1.85 × 10 ⁴
	17 (P _{10s} - equivalent specific current)	51		0.235 mM:0.47 M (1:2000, Li-Na binary)	16.5:1	3.30 × 10 ⁴
	17 (P _{10s} - equivalent specific current)	51		1.88 mM:0.47 M (1:250, Li-Na binary)	1:0 (Na below detection limit)	n.a.
This work	Specific current during extraction (mA/g)	Capacity used during extraction (mAh/g)	Total capacity used (mAh/g)	Initial Li:Na (at%)	Recovered Li:Na (at%)	Selectivity
	(147 mA/g = 1 C)					
L(0)-LN(0.1) _{0.1C}	14.7	14.7	14.7	1 mM:1 M (1:1000)	11.0:1	1.10 × 10 ⁴
L(0)-LN(0.2) _{0.1C}	14.7	29.4	29.4		5.4:1	5.41 × 10 ³
L(0)-LN(0.3) _{0.1C}	14.7	44.1	44.1		3.7:1	3.66 × 10 ³
L(0)-LN(0.4) _{0.1C}	14.7	58.8	58.8		2.0:1	2.05 × 10 ³
L(0)-LN(0.7) _{0.01C}	1.47	102.9	102.9		13.6:1	1.36 × 10 ⁴
L(0)-LN(0.7) _{0.1C}	14.7	102.9			1.7:1	1.68 × 10 ³
L(0)-LN(0.7) _{0.2C}	29.4	102.9			1.1:1	1.12 × 10 ³
L(0)-LN(0.7) _{0.5C}	73.5	102.9			0.4:1	4.15 × 10 ²
L(0.1) _{4C} -LN(0.7) _{0.1C}	14.7	88.2			1.6:1	1.58 × 10 ³
L(0.2) _{4C} -LN(0.7) _{0.1C}	14.7	73.5			2.6:1	2.61 × 10 ³
L(0.3) _{4C} -LN(0.7) _{0.1C}	14.7	58.8			3.5:1	3.50 × 10 ³
L(0.4) _{4C} -LN(0.7) _{0.1C}	14.7	44.1			6.0:1	6.00 × 10 ³
L(0.2) _{4C} -LN(0.7) _{0.2C}	29.4	73.5			1.6:1	1.62 × 10 ³
L(0.2) _{4C} -LN(0.7) _{0.5C}	73.5	73.5			0.6:1	6.50 × 10 ²
L(0.2) _{0.1C} -LN(0.7) _{0.1C}	14.7	73.5			1.9:1	1.94 × 10 ³
L(0.2) _{2C} -LN(0.7) _{0.1C}	14.7	73.5			2.6:1	2.64 × 10 ³
L(0.2) _{6C} -LN(0.7) _{0.1C}	14.7	73.5			2.7:1	2.72 × 10 ³
L(0.2) _{8C} -LN(0.7) _{0.1C}	14.7	73.5			3.3:1	3.26 × 10 ³
L(0.4) _{0.1C} -LN(0.7) _{0.1C}	14.7	44.1			2.7:1	2.74 × 10 ³
L(0.4) _{2C} -LN(0.7) _{0.1C}	14.7	44.1			4.4:1	4.38 × 10 ³
L(0.4) _{6C} -LN(0.7) _{0.1C}	14.7	44.1		9.0:1	9.05 × 10 ³	
L(0.4) _{8C} -LN(0.7) _{0.1C}	14.7	44.1		14.8:1	1.48 × 10 ⁴	

Supplementary Table 8 Summarized channel filling information. Li atoms tend to occupy more channels, with equal fractions of vacancy and Li in each channel.

Phase	Channel condition
Li _{0.125} FP	½ quarter + ½ empty
Li _{0.250} FP	¾ empty + ¼ full
Li _{0.375} FP	½ half (dimer) + ½ quarter
Li _{0.500} FP	All half filled
Li _{0.625} FP	½ half (dimer) + ½ three quarters
Li _{0.750} FP	All three-quarters filled
Li _{0.875} FP	½ full + ½ three-quarters

Supplementary Table 9 Summary of calculated potential difference for Li-Na intercalation of different phases.

Li _x FePO ₄	Potential difference for Li-Na intercalation [eV]
0.000	-1.1676
0.125	-1.1769
0.250	-1.2072
0.375	-1.3164
0.500	-1.3732
0.625	-1.3849
0.750	-1.3435
0.875	-1.4148

Supplementary Table 10 Li and Fe content of the chemically Li-extracted EG-FePO₄ hosts measured by ICP-MS. (Noting that 1. The measurement errors here denote the standard deviations of Li and Fe concentrations for each sample; 2. The average concentrations of Li and Fe are used to calculate the molar ratio for each sample; 3. Li/Fe_{ave} (at. %) denote the average Li/Fe molar ratio of the three samples.)

EG-FePO ₄	Label	Li (ppb)	Fe (ppb)	Li/Fe (at. %)	Li/Fe _{ave} (at. %)
Raw	S1	7.405 ± 0.055	246.620 ± 1.988	24.0%	23.5%
	S2	7.843 ± 0.064	267.724 ± 1.607	23.4%	
	S3	19.095 ± 0.275	662.835 ± 4.525	23.0%	

Supplementary Table 11 Fitted phase fractions of Supplementary Figure 24 with the calculated weighted sum of Li.

EG-FePO ₄	LFP	L0.875FP	L0.75FP	L0.625FP	L0.5FP	L0.375FP	L0.25FP	L0.125FP	FP	Intercalated Li	Weighted sum of Li
Raw	0.08255	0.10463	0.01853	0	0	0.11015	0.10872	0.245	0.33041	0	0.28711
After recovery	0.08856	0.1	0.01685	0	0	0.10857	0.12296	0.23901	0.32405	0	0.29003
L(0.2) _{4c}	0.1117	0.09476	0.00316	0.05839	0.03014	0.13481	0.09826	0.2001	0.26867	0.2	0.34868

Supplementary Table 12 Summarized refined lattice parameters for the three different FePO₄ samples.

	Comm-LiFePO ₄	Synthesized-LiFePO ₄	EG-LiFePO ₄		Comm-FePO ₄	Synthesized-FePO ₄	EG-FePO ₄
a (Å)	10.321	10.347	10.320	a (Å)	9.818	9.819	9.830
b (Å)	6.005	6.007	6.000	b (Å)	5.792	5.798	5.795
c (Å)	4.691	4.700	4.701	c (Å)	4.781	4.785	4.780
α	90			α	90		
β				β			
γ				γ			

Supplementary Table 13 Electrode resistances for the carbon-coated FePO₄ electrode wo/w 3nm TiO₂ coating obtained from equivalent circuit fitting of EIS results.

(Noting that $CPE1 = \frac{1}{Q1(j\omega)^{a1}}$, $CPE2 = \frac{1}{Q2(j\omega)^{a2}}$, $ZW = \sigma\omega^{-1/2} - j\sigma\omega^{-1/2}$ and the error is calculated using the Levenberg-Marquardt algorithm, which can be assimilated to a standard deviation. It gives an estimate of the relevancy of the parameter. If the error is very high it means that a great variation of the parameter will not affect very much the quality of the fit. Hence, the considered parameter is not critical in the minimization process.)

		wo TiO ₂	w TiO ₂
R _s (Ohm)		5.22 ± 0.17	5.48 ± 0.197
R ₁ (Ohm)		21.06 ± 0.359	9.70 ± 6.085
R ₂ (Ohm)		19.30 ± 1.388	22.64 ± 0.323
CPE1	Q1 (F·s ^(a1-1))	0.02 ± 0.003	0.50 ± 0.307
	a1	0.78 ± 0.592	0.87 ± 0.592
CPE2	Q2 (F·s ^(a2-1))	0.03 ± 0.001	0.01 ± 0.001
	a2	0.97 ± 0.83	0.73 ± 0.528
Zw	σ (Ohm·s ^(-1/2))	24.20 ± 1.268	12.4 ± 1.502

Supplementary Table 14 Recovered Li/(Li+Na)_{net} ratios of the carbon-coated FePO₄ electrode wo/w 3nm TiO₂ coating using 20% Li seeding (Error bars representing the standard deviation of three replicate measurements).

L(0.2)_{4C}-LN(0.7)_{0.1C}

	wo TiO ₂	w TiO ₂
Li/(Li+Na) _{net}	0.73 ± 0.01	0.74 ± 0.01

Total Energy Calculation

Total energies of structures were determined using DFT calculations with the project augmented-wave (PAW)⁶ approach as implemented in the Vienna ab initio Simulation package (VASP)^{7,8}. A plane wave energy cutoff of 520 eV and a Gamma-centered k-point grid with a k-point density of at least 1000/(number of atoms in unit cell) was used. The Perdew-Burke-Ernzerhof (PBE)⁹ generalized-gradient approximation (GGA)¹⁰ exchange-correlation functional with the GGA+U extension. A U value of 5.3 eV was used for Fe which was determined by the Materials Project by fitting experimental binary formation enthalpies of TM oxides¹¹⁻¹³. All structures were fully optimized until the energy was converged to within 10⁻⁵ eV per supercell and the forces on each atom were less than 0.02 eV/Angstroms.

Structure Search

DFT energies of the Li_xNa_yFePO₄ (0 ≤ x+y ≤ 1) system were fit using a cluster expansion (CE) model to search for low-energy configurations given a maximum supercell size. The CE formalism is a well-established approach for studying ordering in alloys¹⁴⁻¹⁷. In the CE model the mixing enthalpies of the structures are parametrized using clusters, α . The mixing enthalpy of each structure's configuration σ is fit using a sum of weighted cluster correlation functions based on the products of occupation variables σ_i . J_α is the effective cluster interaction (ECI) for the cluster α . Using a chosen set of clusters, the energy of a structure with a configuration σ given by occupation variables σ_i is predicted using Eq. 1.

$$\Delta E(\sigma) = \sum_{\alpha} m_{\alpha} J_{\alpha} \prod_{i \in \alpha'} \sigma_i \quad (1)$$

where m_{α} is the multiplicity of cluster α , which is determined by the symmetry of the parent lattice. In this study two cluster expansions were fit, one for the ternary system and a second one focusing on the Li-vacancy edge of the Li_xNa_yFePO₄ system. In total, 506 DFT energies were calculated, with 161 of those on the Li-vacancy edge. The 506 structures show that the only intermediate structure stable with respect to the terminal compositions LiFePO₄, NaFePO₄ and FePO₄ is Na_{0.66}FePO₄. From the set of 161 structures on the Li-vacancy edge, low energy configurations with greater separation of structural Li atoms and vacancies were selected for seven intermediate Li concentrations. The selected structures were later used to calculate the difference between Li and Na intercalation potentials. The search for low energy configurations considered all supercells containing at most 86 atoms. In this work, the ICET package was used for the construction of the CE model¹⁸. A large cluster space (2280) with clusters up to the fourth order (quadruplets) were considered, and the Automatic relevance determination regression (ARDR) algorithm with regularization parameter, $\lambda = 15000$, was used to optimize a sparse set of clusters for the CE model.

Supplementary Note 2: Deconvolution of solid-solution fraction from diffraction patterns

To quantify the solid-solution fraction in Li-seeded FePO₄, we fit the obtained X-ray diffraction patterns to a number of Gaussians, following previous work^{19,20}. The standard LeBail refinement was only possible for the end phases of LiFePO₄ and FePO₄ because the lattice parameters of all intermediate phases are completely interchangeable²¹. Fortunately, Vegard's law has been experimentally demonstrated to be valid in the case of Li_xFePO₄^{20,22-24}. Generally, we can first calculate the corresponding lattice parameters for all intermediate phases with a linear combination of the refined end phases for LiFePO₄ and FePO₄, and then get the peak positions for all intermediate phases. Detailed steps are described below:

S1: LeBail refinement of the end phases of LiFePO₄ and FePO₄ (Supplementary Figure 4): The fitted lattice parameters for LiFePO₄ and FePO₄ are summarized in Supplementary Table 2, denoted by green and purple, respectively.

S2: Applying the Vegard's law to calculate the lattice parameters for intermediate phases (Supplementary Table 2): The deconvolution of a pattern using an infinite number of phases was assumed to be impossible. Thus, we deconvoluted the patterns for the seven intermediate phases of composition Li_xFePO₄, $x = 0.125/0.250/0.375/0.500/0.625/0.750/0.875$ with the space group parameter being a linear combination of the refined end phases for LiFePO₄ and FePO₄ (lattice parameters *a*, *b*, and *c* for space group *Pnma* for LiFePO₄ are 10.347, 6.007 and 4.700 Å, and those for FePO₄ are 9.819, 5.798 and 4.785 Å).

S3: Calculating the peak positions according to the lattice parameters in *b* with GSAS II software: We are using (211) and (020) peaks as characteristic peaks for the fitting, and the positions are summarized in Supplementary Table 3.

S4: Calculating (211) and (020) area ratios: The LeBail refinement of the FePO₄ pattern showed that the ratio between the (211) and the (020) reflection areas is 0.38 (Supplementary Figure 4). Since the (211) peak and (020) peak in LiFePO₄ are too close to distinguish, we use 0.23 as the area ratio according to the reference²⁰. Area ratios of all intermediate phases also follow the linear combination of these two end-up phases, which are summarized in Supplementary Table 4.

S5: Normalization of areas: The scattering factors of LiFePO₄ and FePO₄ differ. Therefore, all areas were normalized to the area of LiFePO₄ by dividing the area of FePO₄ by a factor of 1.24²⁰.

S6: Fitting the XRD spectra with nine species: two end phases, FePO₄ and LiFePO₄, and seven intermediate phases. The difference of state of charge (SOC) between two adjacent phases is set as 12.5%. And each phase will contribute two peaks, one is (020) peak and another one is (211) peak. So totally, we need to fit the band with 18 Gaussians. We can then get all the areas of peak (211) and (020) for each Li_xFePO₄ phase ($x = 0/0.125/0.250/0.375/0.500/0.625/0.750/0.875/1$).

S7: The phase fraction of each Li_xFePO₄ phase ($P.F._{Li_xFP}$) is defined to be:

$$P.F._{Li_xFP} = \frac{[A_{Li_xFP}(211) + A_{Li_xFP}(020)] \cdot x + \frac{[A_{Li_xFP}(211) + A_{Li_xFP}(020)] \cdot (1-x)}{1.24}}{\sum\{[A_{Li_xFP}(211) + A_{Li_xFP}(020)] \cdot x + \frac{[A_{Li_xFP}(211) + A_{Li_xFP}(020)] \cdot (1-x)}{1.24}\}}$$

where $A_{Li_xFP}(211)$ is the area of Li_xFePO₄ (211) peak and $A_{Li_xFP}(020)$ is the area of the Li_xFePO₄ (020) peak.

Supplementary Note 3: Potential reasons for the deviations of calculated weighted sum of Li from fitting

As shown in Supplementary Figure 5 and Supplementary Table 5, we saw deviations in the calculated weighted sum of Li compared to our seeding range. We plotted the calculated weighted sum of Li from XRD fittings versus the electrochemically intercalated Li amount, as shown in Supplementary Figure 6. The relationship between the calculated weighted sum of Li and the depth of intercalation has good linearity ($R^2 = 0.999$). The deviation of the XRD fitted Li amount from electrochemical seeding amount indicates the possibility of unidentified system error. Even with error, this good linearity supports our analysis of the correlation of Li selectivity to Li solid solution phases since the error cannot be randomly affecting either the low-Li or high-Li solid solution phase fractions. Otherwise, there will not be a good linearity.

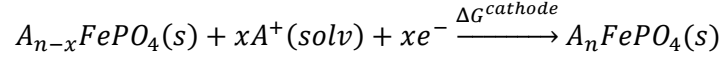
We think there could be two reasons that cause the deviations:

1. In order to have a quantitative measurement, we need to do LeBail refinement for the whole XRD patterns. However, the standard LeBail refinement was possible only for the end phases of LFP and FP because the lattice parameters of all intermediate phases were completely interchangeable²⁰. With the help of Vegard's law, we could achieve a calculation of Li from XRD patterns. The intermediate phases do not correspond to a single phase of a specific concentration but all Li concentrations (x) in LiFePO_4 , $0 < x < 1$ during the transition²⁵. In other words, the more accurate deconvolution of the XRD intensity band requires an infinite number of phases, which is assumed to be impossible and impracticable, and could also lead to overfitting issues. Since only nine different phases of state of charge were chosen to deconvolute the XRD patterns, this simplification assigned the other intermediate phases to the nine chosen ones, which could cause deviations of the calculated weighted sum of Li.
2. We find out that the intensity contributions from the polyvinylidene difluoride (PVDF), super P, and carbon cloth substrate could also introduce deviations by raising the background intensity, especially under the low depth of intercalation. PVDF and super P are indispensable binders and conductive additives for the preparation of FePO_4 electrodes. The flexible carbon cloth is a good choice considering manufacturing and practical use. We then tried mirror polished glassy carbon with flatter surface as the substrate. The new glassy carbon substrate decreases the deviations caused by porous structures of carbon cloth. As shown in Supplementary Figure 7 and Supplementary Table 6, we achieved a better agreement between the calculated weighted sum of Li and the depth of intercalation, which also shows a good linear relationship in Supplementary Figure 8a. We also witnessed a similar monotonically increasing trend of high-Li SS phases with increased seeding range under 4C (588 mA/g) in Supplementary Figure 8b, while the low-Li SS phases still did not correlate with the increasing Li seeding range.

At this stage, although we witnessed some deviations of the calculated weighted sum of Li from deconvolution results, the general trend is repeatable and reasonable. Moreover, for the consistency of comparisons and practical feasibility, all the samples are tested on carbon cloth substrate unless specified.

Supplementary Note 4: Calculating Li-Na potential difference with respect to solvated ions

For the structures on the Li-vacancy edge of the $\text{Li}_x\text{Na}_y\text{FePO}_4$ system the difference in potential for intercalating Li vs Na was calculated by determining the energy contribution from the electrochemical metal-ion insertion reaction shown in the equation below:



The preference of Li vs. Na is compared by calculating the concentration corrected chemical potential of Li and Na^{26} . To be specific,

$$\Delta G_{\text{solvated},A^+}^{\text{cathode}} = -x\Delta G_{\text{solv}}^{A^+} - xIE - \Delta G_{\text{atom},A}^{\text{cathode}} + 0.059\log\left(\frac{1}{[A]^x}\right)$$

where $\Delta G_{\text{atom},A}^{\text{cathode}}$ is the energy to extract an isolated atom A from the cathode, IE is the ionization energy of A, and $\Delta G_{\text{solv}}^{A^+}$ is the solvation energy of A^+ . Precisely, according to the literature, the ionization energy for Li and Na are 5.39171 eV and 5.13908 eV respectively²⁷. Meanwhile, the solvation energy for Li^+ and Na^+ are 5.389 eV and 4.198 eV respectively²⁸. The Li and Na potentials were calculated at 8 different Li-ion concentrations (0, 0.125, 0.25, 0.375, 0.5, 0.625, 0.75, and 0.875). At each composition, among the low energy configurations the configurations with greater separation of structural Li atoms and vacancies were selected. This is because the thermodynamically stable state of these compositions is a decomposition into LiFePO_4 and FePO_4 . For each selected configuration a single Li or Na atom was placed on a vacancy site. If there were vacancy sites with different number of first, second, third structural Li nearest neighbors, two different calculations were performed. One where the added Li or Na atom was placed in order to maximize the proximity of structural Li atoms, and another where the Li or Na atom was placed as far away from the structural Li atoms as possible. Of the two resulting energies, the one with the lower energy was used for the Li and Na potential calculation. All configuration corresponded to 56 atom supercells, if all vacancies were filled, therefore with the addition of a single Li or Na atom x in the above equations is 0.125.

Then the Li-Na potential difference for each phase can be calculated using the following equation:

$$\Delta G_{\text{Li-Na}}^{\text{Li}_x\text{FePO}_4} = \Delta G_{\text{solvated},\text{Li}^+}^{\text{Li}_x\text{FePO}_4} - \Delta G_{\text{solvated},\text{Na}^+}^{\text{Li}_x\text{FePO}_4}$$

The calculated Li-Na intercalation potential differences for each phase are summarized in Supplementary Table 9. We also provided channel filling information for each intermediate phase in Supplementary Table 8 for reference. More negative Li-Na potential difference shows that the Li-ion intercalation is preferred to Na-ion intercalation.

Supplementary Note 5: Roles of surface carbon and TiO₂ coatings

Surface carbon coating was conducted for each FePO₄ sample by sugar pyrolysis, followed by 3 nm TiO₂ coating over the entire electrode. 3 nm TiO₂ was coated onto the FePO₄ electrodes using atomic layer deposition (ALD) at 100°C, 0.645 Å/cycle with tetrakis(dimethylamido)titanium (IV) and H₂O as precursors. We discussed the roles of surface carbon and TiO₂ coatings below for reader's information:

1. The battery cycling performance comparison among Bare, Carbon-coated, and TiO₂-Carbon-coated FePO₄ electrodes is summarized in Supplementary Figure 26. Under 0.1C (14.7 mA/g), the TiO₂-Carbon-coated FePO₄ electrode delivered a similar specific capacity (147 mAh/g) with only Carbon-coated FePO₄ electrode (151 mAh/g), while the Bare-FePO₄ electrode without either coating delivered a much worse specific capacity (120 mAh/g; Note: bare particles were annealed under the same condition without mixing with sucrose). Surface carbon coating does help improve the performance of LiFePO₄ electrodes.
2. For the role of TiO₂ coating, as shown in Supplementary Figure 27a, without TiO₂ coating, the carbon-coated FePO₄ together with carbon cloth substrate is highly hydrophobic. After coating the electrode with TiO₂, the 10 μL water immediately infiltrated the electrode surface. Several pre-wetting steps can be avoided using TiO₂-Carbon-coated FePO₄ electrodes. We also conducted electrochemical impedance spectroscopy measurements in 1M LiCl aqueous solution. Supplementary Figure 27b shows the Nyquist plots for the carbon-coated FePO₄ wo/w the 3 nm TiO₂ coating with the equivalent circuit shown in the inset. The resistor R_s corresponds to the electrolyte resistance. The resistors R₁ and R₂ paralleled with the constant phase element (CPE) account for the contact impedance and charge transfer impedance, respectively. The ion diffusion in the host material is described with the Warburg element (Z_w). As shown in Supplementary Figure 27b, the data from the equivalent circuit well fit the impedance data for both electrodes. The values for the different resistances obtained from the fitting are listed in Supplementary Table 13. As shown in the table, the electrolyte resistance (R_s) and charge transfer impedance (R₂) are almost the same for the carbon-coated FePO₄ wo/w the TiO₂ coating. The contact impedance (R₁) of the electrode without TiO₂ coating is more than double the value of the electrode with TiO₂ coating. Therefore, the TiO₂ coating can reduce the contact resistance as well.
3. We further evaluated the effect of TiO₂ coating on the seeding process. Supplementary Figure 28 shows the XRD patterns of the carbon-coated FePO₄ electrode wo/w TiO₂ coating after 20% Li seeding under 4C (588 mA/g). There is little difference for both obtained and fitted patterns. The calculated solid solution fraction (SSF) for the electrode without or with TiO₂ coating are 0.429 and 0.428, respectively, which is similar. And the recovered Li/(Li+Na) ratios for the following Li extraction step are almost the same (Supplementary Table 14). Without TiO₂, Li/(Li+Na)_{net} is 0.73 ± 0.01, and with TiO₂, Li/(Li+Na)_{net} is 0.74 ± 0.01. Therefore, the above results show that the TiO₂ coating will not affect SSF generated in the seeding process, as well as the following Li extraction performance. Long term corrosion resilience can be a benefit of TiO₂ coating.

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